



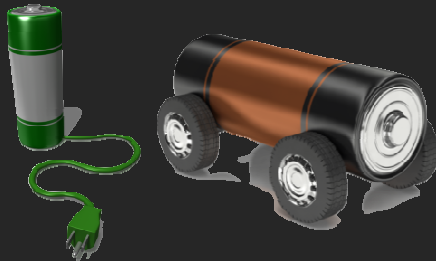


*Pregl colloquium*  
**NIC**

Ljubljana, Slovenia  
December 14, 2016



# **Mesostructure-performance relationships in batteries: challenging the dogma with multiscale computations**



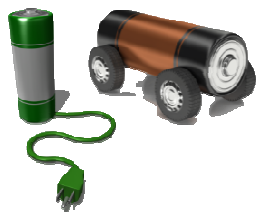
**Prof. Alejandro A. Franco<sup>1,2,3,4</sup>**

<sup>1</sup>LRCS, Université de Picardie Jules Verne & CNRS – Amiens, France

<sup>2</sup>Réseau sur le Stockage Electrochimique de l'Energie (RS2E)

<sup>3</sup>ALISTORE European Research Institute

<sup>4</sup>Institut Universitaire de France



# LABORATOIRE DE REACTIVITE ET CHIMIE DE SOLIDES



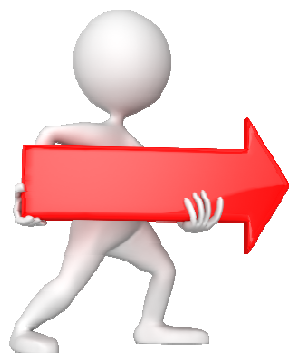
New building (rue St. Leu, since 2017)



**LRCS (UMR UPJV/CNRS 7314)  $\cong$  80 people**

(Director: M. Morcrette)

- **Electrochemical conversion and storage**
- Solid state materials chemistry
- Nanostructured materials
- Advanced characterization techniques
- Theory

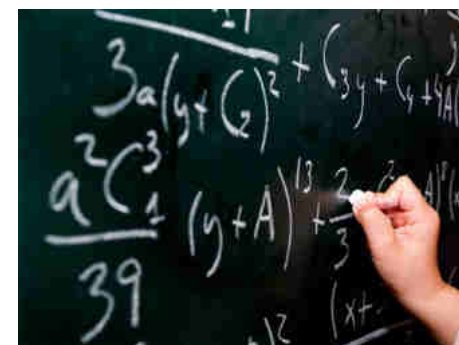
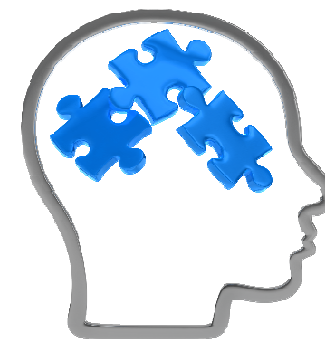
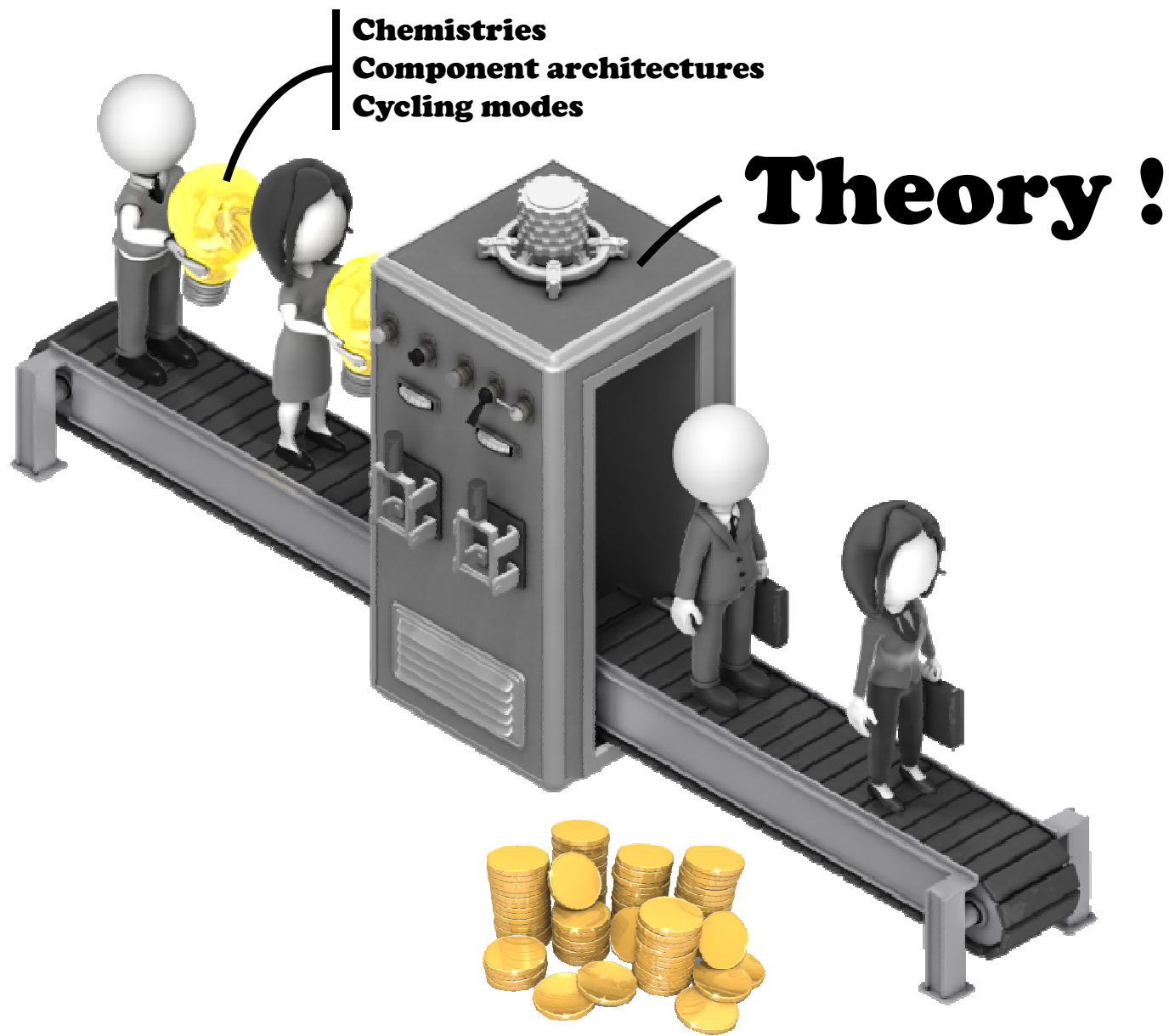


→ **LRCS (Prof. J.M. Tarascon):** lead the foundation of the national **RS2E** network and of the **ALISTORE** European Research Institute.



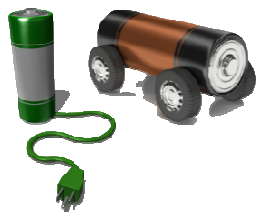
*Prof. Alejandro A. Franco*  
Mesostructure-performance relationships in batteries...  
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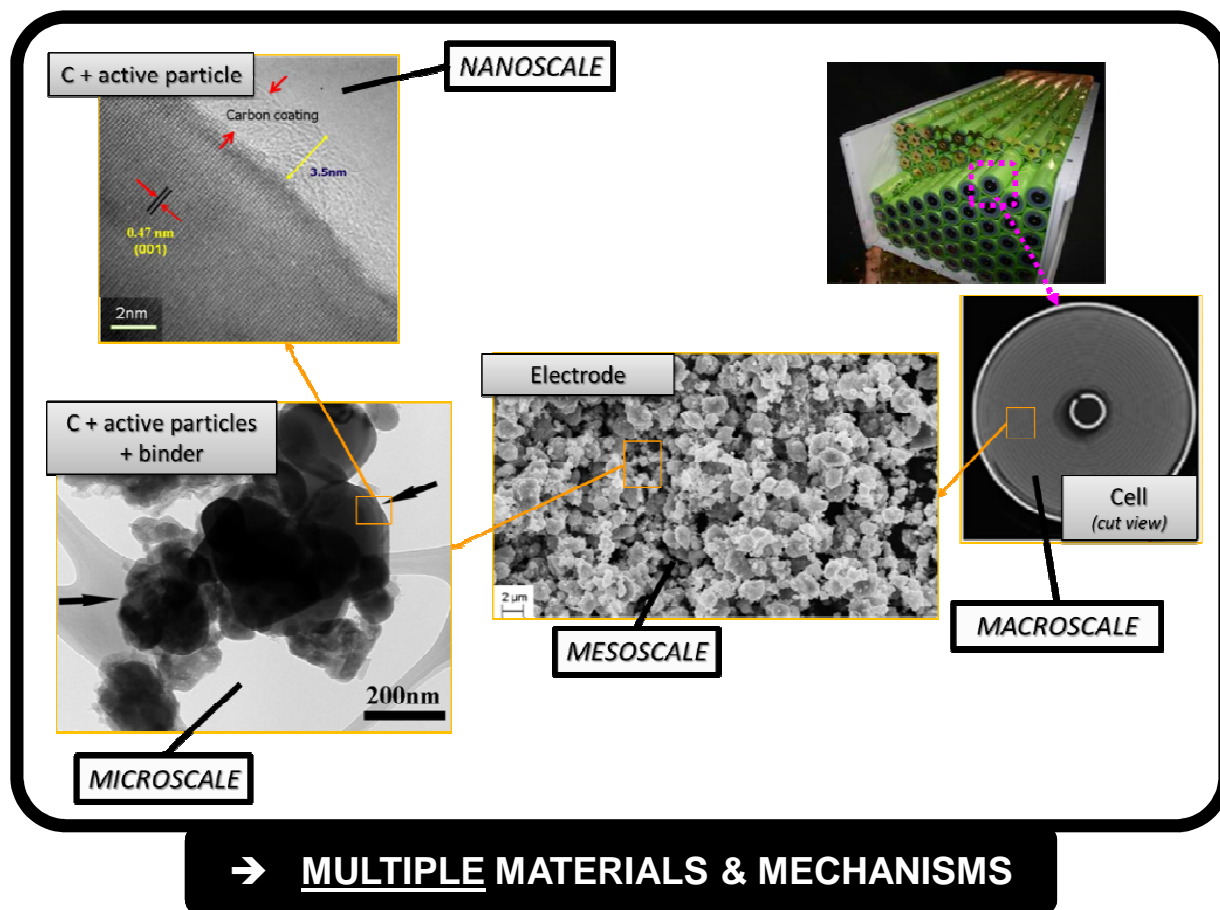


***In silico* experimentation**

A.A. Franco in: A.A. Franco, M.L. Doublet, W. Bessler, Eds., *Physical Multiscale Modeling and Numerical Simulation of Electrochemical Devices for Energy Conversion and Storage*, Springer London (2016).



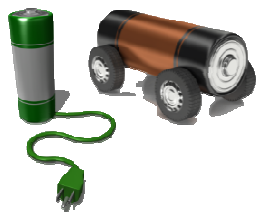
# MULTISCALE COMPLEXITY IN BATTERIES



A.A. Franco, *RSC Adv.* **3** (2013) 13027.

A.A. Franco, in: *Encyclopedia of Applied Electrochemistry*, G. Kreysa, K. Ota, R. F. Savinell (Eds.), Springer, New York (2014).

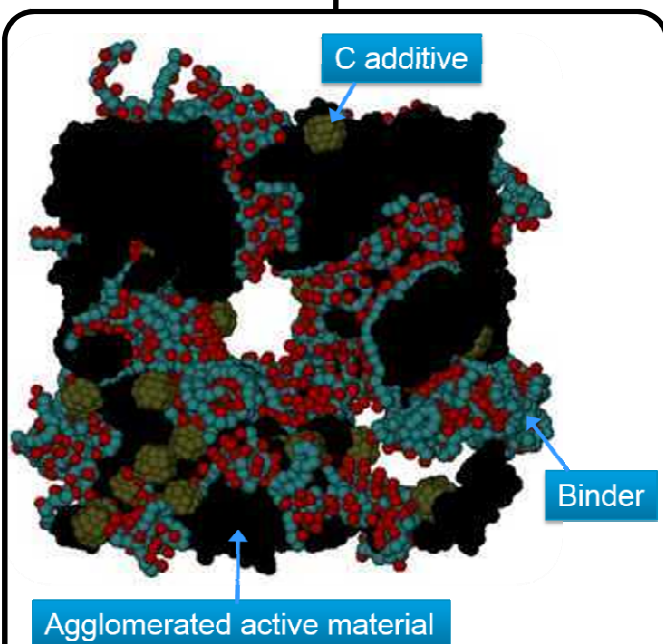
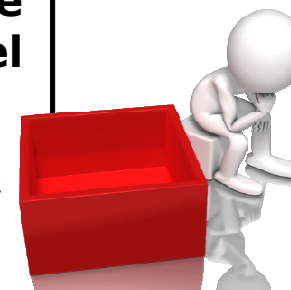
A.A. Franco, M.L. Doublet, W. Bessler, Eds., *Physical Multiscale Modeling and Numerical Simulation of Electrochemical Devices for Energy Conversion and Storage*, Springer London (2016).



# OUR MULTISCALE MODELING PLATFORM

➤ **Flexible computational platform (adaptable to a wide diversity of systems, e.g. Li-Ion, Na-Ion, Li-Air, Li-S, Fuel Cells, etc.)**

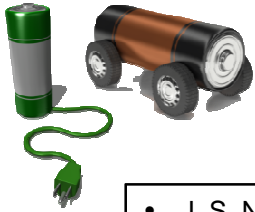
- ↳ to investigate electrode mesoscale properties impact on cell performance;
- ↳ to discover optimal compositions, architectures and cycling modes.



**Mesoscopic  $\approx$  few  $\mu\text{m}$**



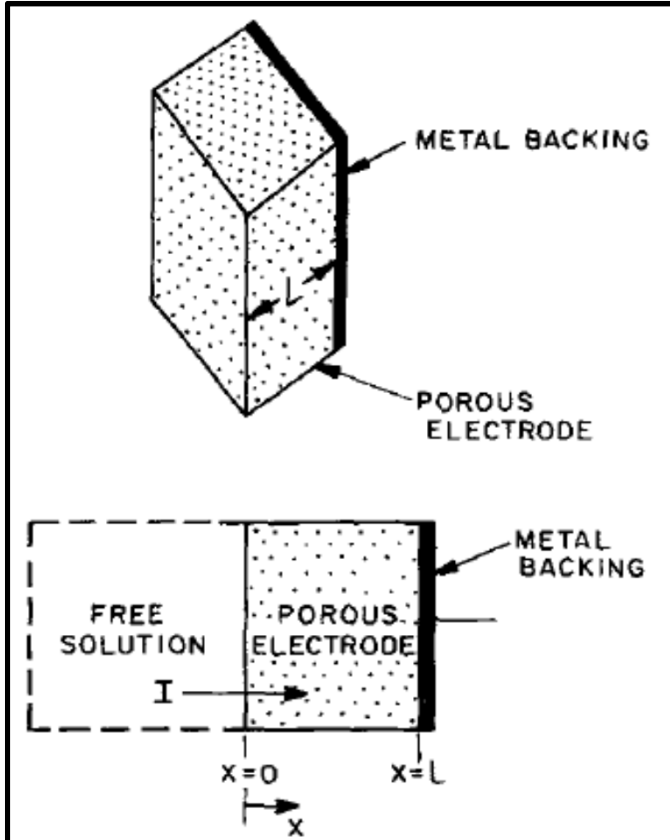
From left to right: R. Zhao, Dr. M. Quiroga, A. Torayev, G. Shukla, Y. Yin, A. Geng, Prof. A..A Franco, M. Maiza, V. Thangavel, R. Andersson, C. Gaya, A. Shodiyev.



# STATE-OF-THE-ART MATHEMATICAL MODELING OF RECHARGEABLE BATTERIES

- J. S. Newman, C. W. Tobias, *J. Electrochem. Soc.*, **109** (12) (1962) 1183.
- J. S. Newman, W. Tiedemann, *AIChE Journal*, **21** (1) (1975) 25.

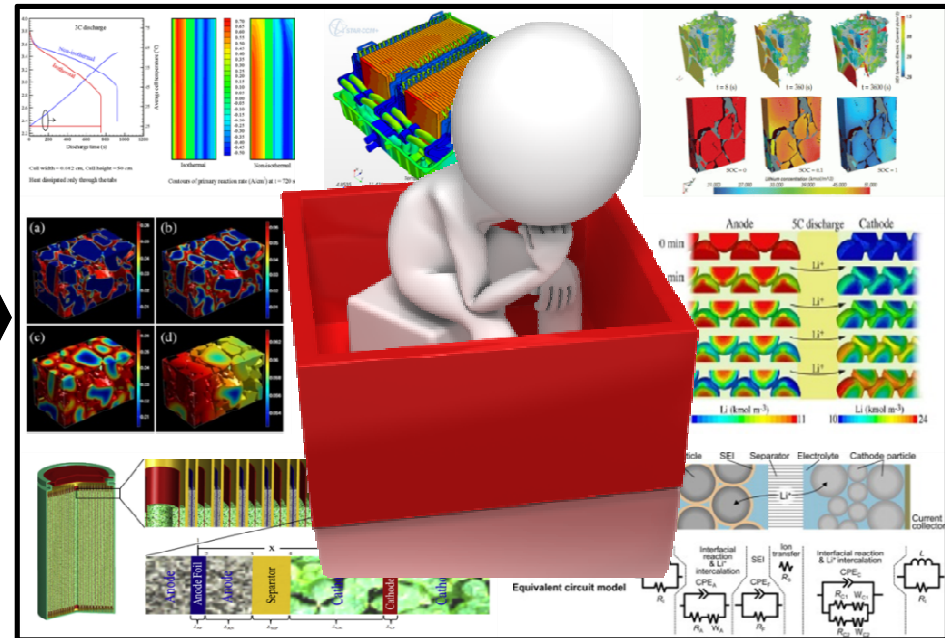
POROUS ELECTRODE THEORY



$$\vec{J}_{Li^+}(\vec{x}, t) = -D_{Li^+} \nabla C_{Li^+}(\vec{x}, t)$$

$$D_{Li^+} = \epsilon^v D_{Li^+}^{bulk}$$

~ 50 years of rechargeable battery models based on Newman's approach...

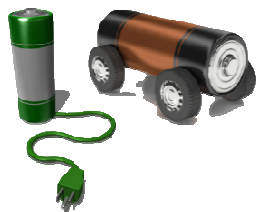


→ Macroscopic description of the porosity and the tortuosity.

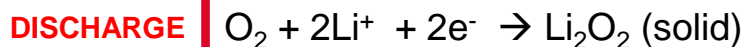
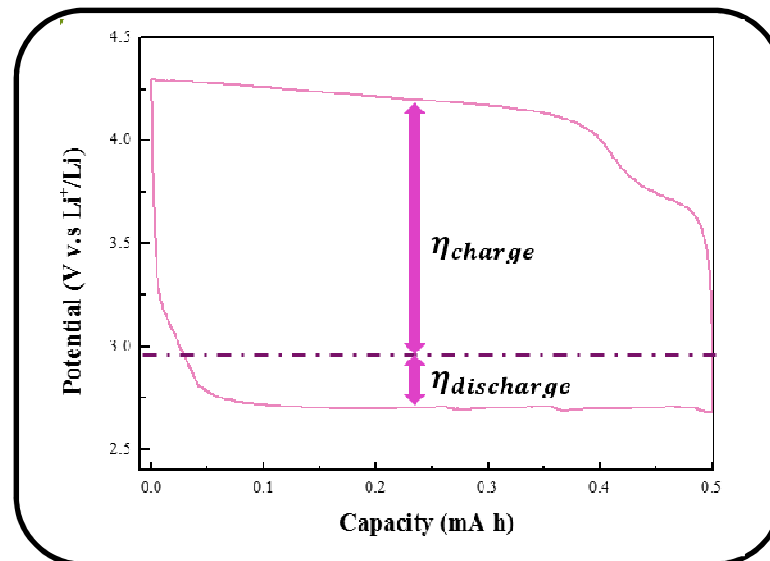
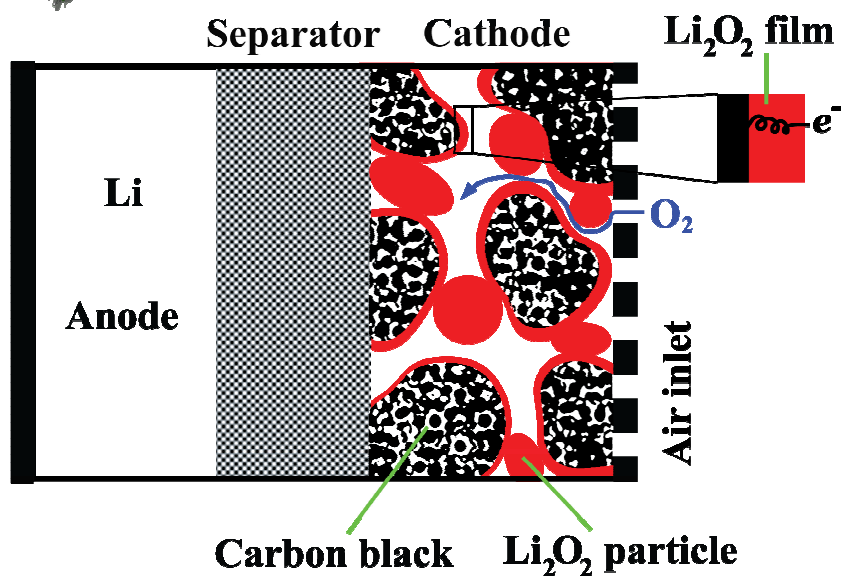
# 1. LITHIUM-O<sub>2</sub> BATTERIES








# LITHIUM AIR BATTERIES: PRACTICAL ISSUES



$O_2$   AIR

Low Round-trip Efficiency:

$$RTE = \frac{E_{out}}{E_{inp}}$$

$$E = Q \times U$$

RTE of LAB: <70% (LIB: > 90%)

Electronic transport

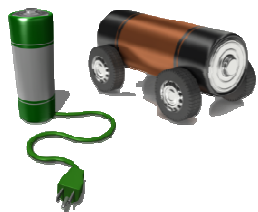
Ionic transport

Oxygen solubility & diffusivity

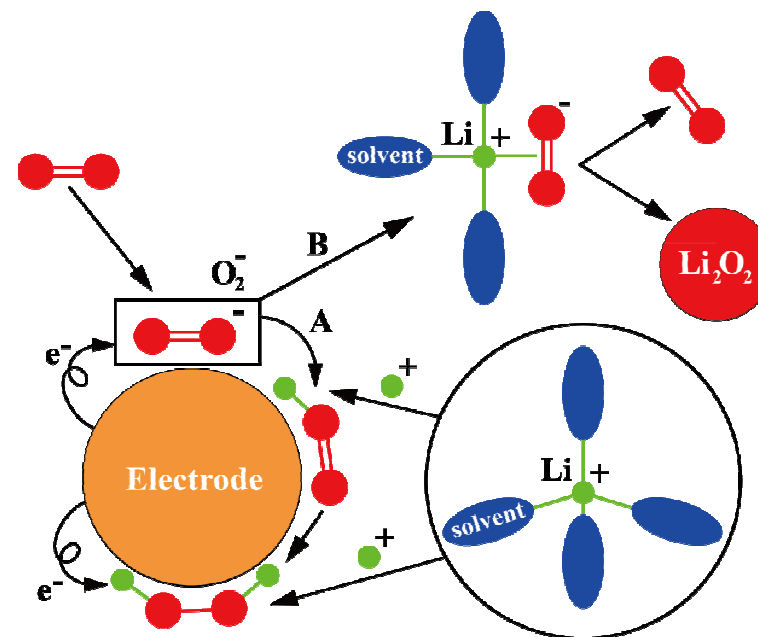
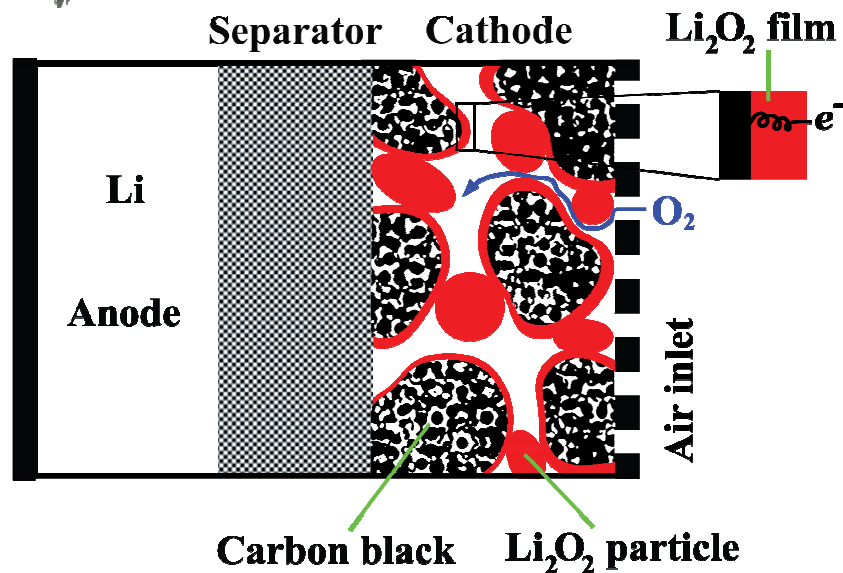
Pore clogging

Electrode passivation

Materials degradation



# OXYGEN REDUCTION REACTION (ORR) @ LI-O<sub>2</sub> BATTERIES



**Route A: Insulating thin film formation on the active surface**

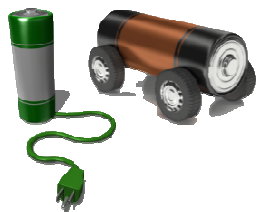
|                    |   |            |
|--------------------|---|------------|
| <b>Consequence</b> | Decrease of oxygen diffusion coefficient: | <b>Yes</b> |
|                    | Consumption of active surface area:       | <b>Yes</b> |

**Route B: Solution phase nucleation-growth of Li<sub>2</sub>O<sub>2</sub> particles**

|                    |   |            |
|--------------------|---|------------|
| <b>Consequence</b> | Decrease of oxygen diffusion coefficient: | <b>Yes</b> |
|                    | Consumption of active surface area:       | <b>No</b>  |

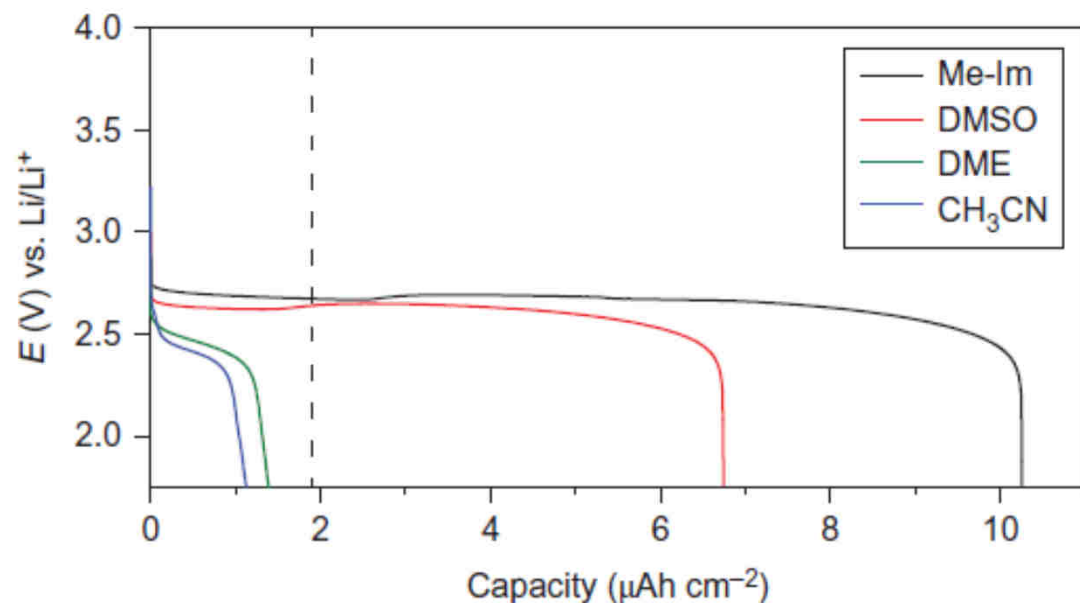
A.A. Franco, K.H. Xue, *ECS J. Solid State Science and Tech.*, **2** (10) (2013) M3084.

L. Johnson, C. Li, Z. Liu, Y. Chen, S. A. Freunberger, P. C. Ashok, B. B. Praveen, K. Dholakia, J.-M. Tarascon, and P. G. Bruce, *Nature Chemistry* **6** (2014) 1091.

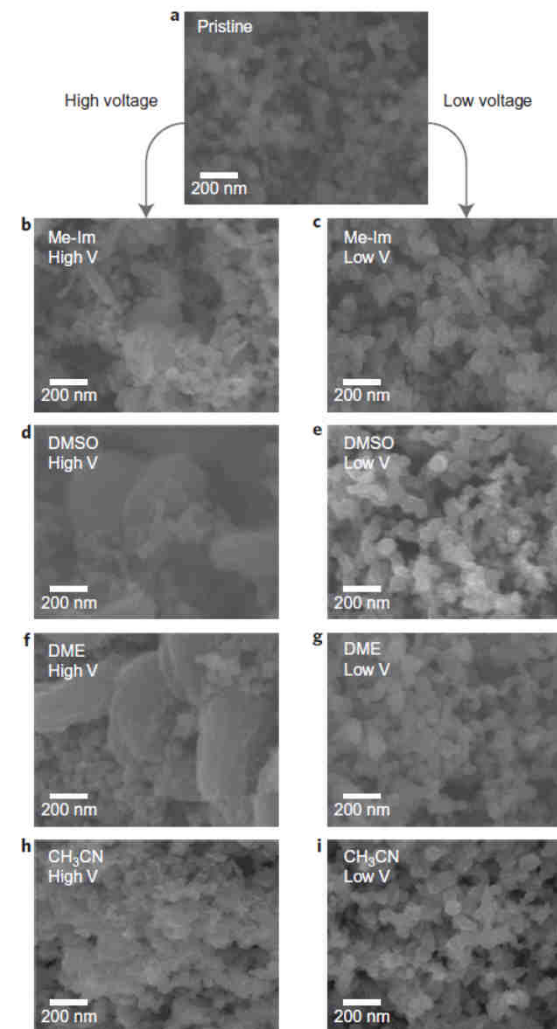


# SOLUTION PHASE VS. THIN FILM ORR MECHANISMS

→ Solvent influences the capacity and the  $\text{Li}_2\text{O}_2$  deposit morphology.



L. Johnson, C. Li, Z. Liu, Y. Chen, S. A. Freunberger, P. C. Ashok, B. B. Praveen, K. Dholakia, J.-M. Tarascon, and P. G. Bruce, *Nature Chemistry* **6** (2014) 1091.



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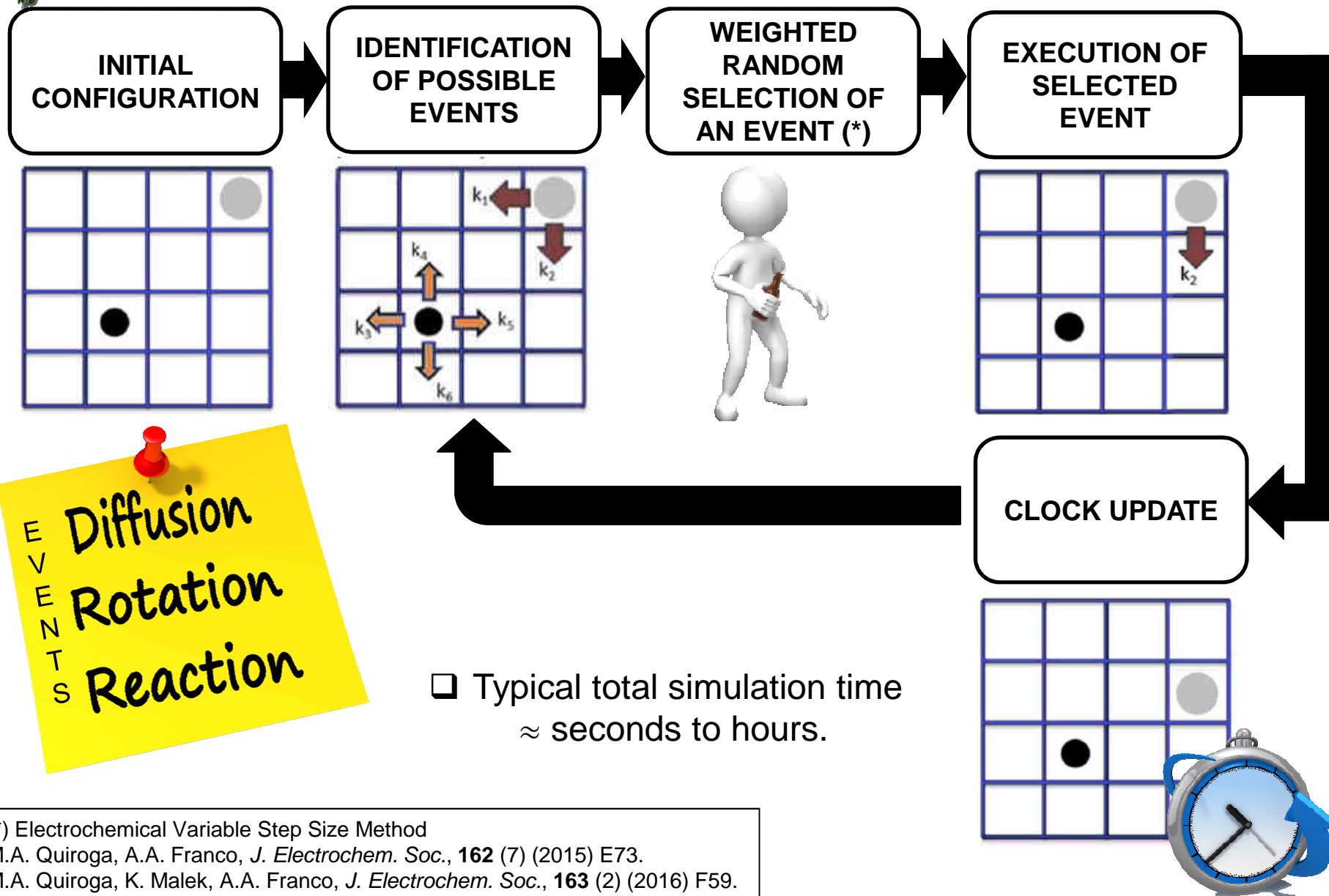
*Monte Carlo Electrochemistry  
Simulation Software for Innovation*

**MESSI**

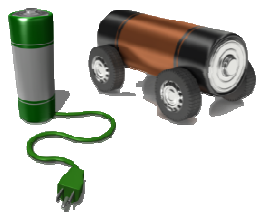




# KINETIC MONTE CARLO MODEL: LINKING CHEMISTRY WITH REACTIONS & DIFFUSION



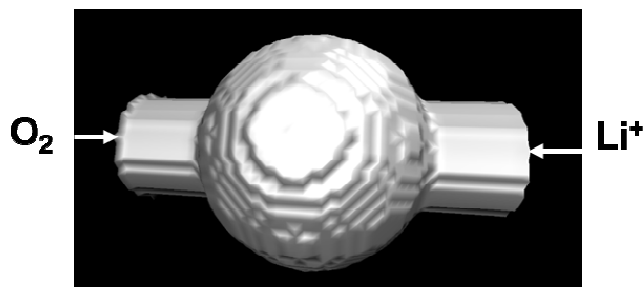
(\*) Electrochemical Variable Step Size Method  
M.A. Quiroga, A.A. Franco, *J. Electrochem. Soc.*, **162** (7) (2015) E73.  
M.A. Quiroga, K. Malek, A.A. Franco, *J. Electrochem. Soc.*, **163** (2) (2016) F59.



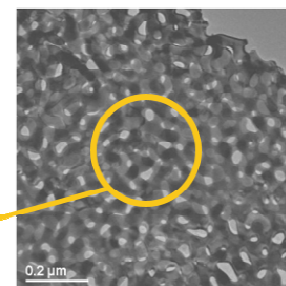
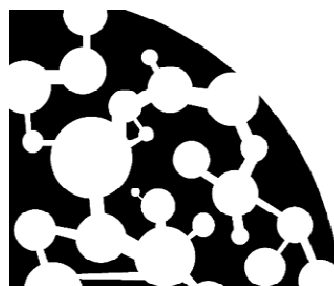
# NANOPORE (1/5): KMC MODELING OF THE ORR

## GEOMETRICAL CONSIDERATIONS

Pore size: 10-30 nm

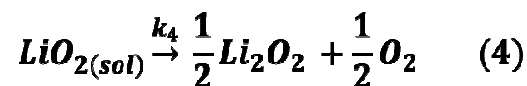
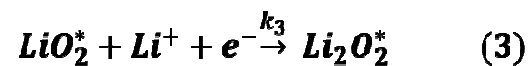
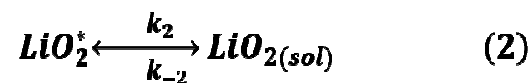
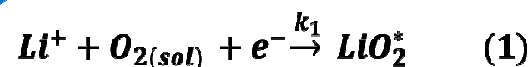
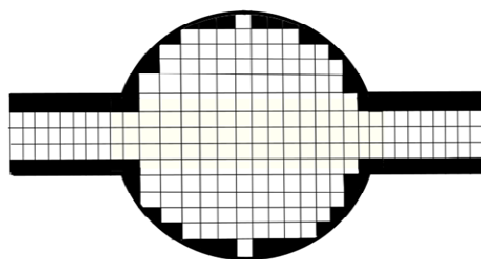


NanoPorous Gold Electrode



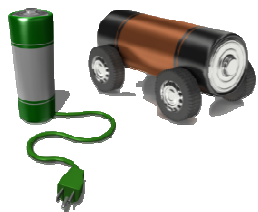
Z.Peng *et al.* *Science* 337, 563–566 (2012)

Grid size: 5 Å



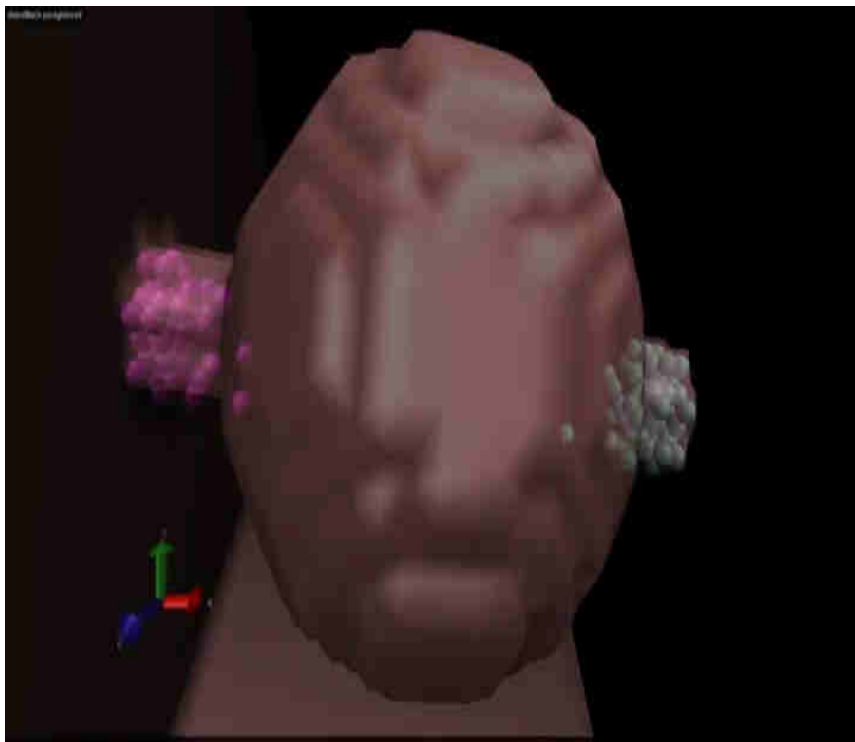
## REACTIONS

G. Blanquer, Y. Yin, M.A. Quiroga, A.A. Franco, *J. Electrochem. Soc.*, **163** (3) (2016) A329.

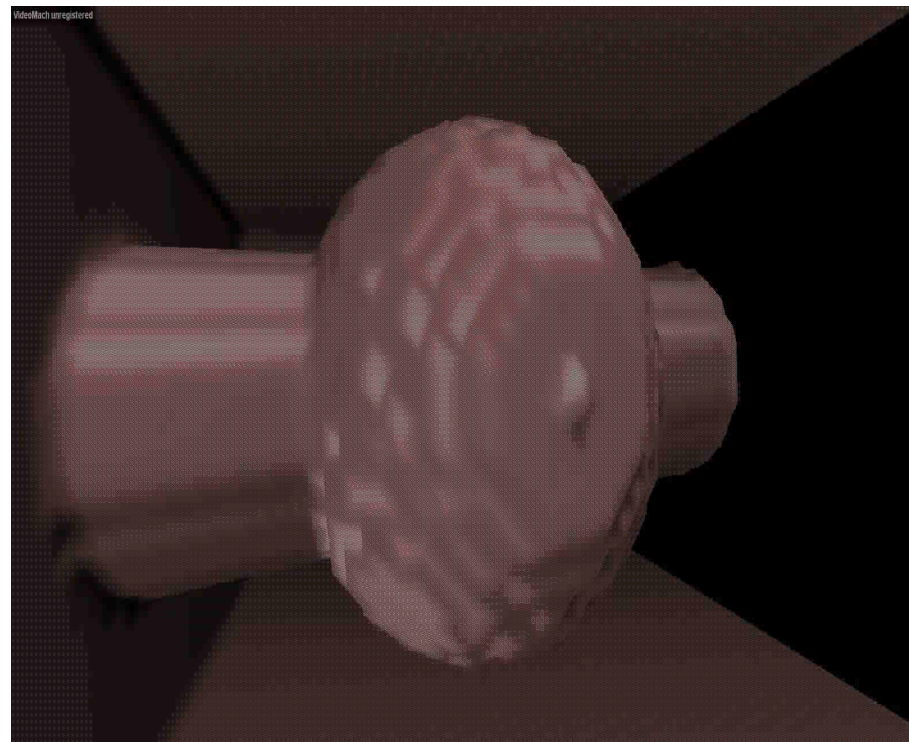


## NANOPORE (2/5): KMC MODELING OF THE ORR

Li<sup>+</sup> and O<sub>2</sub> transport



Li<sub>2</sub>O<sub>2</sub> formation

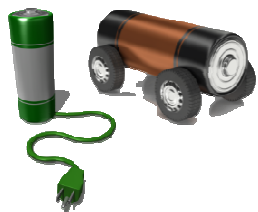


G. Blanquer, Y. Yin, M. Quiroga, A.A. Franco, *J. Electrochem. Soc.*, **163** (3) (2016) A329.

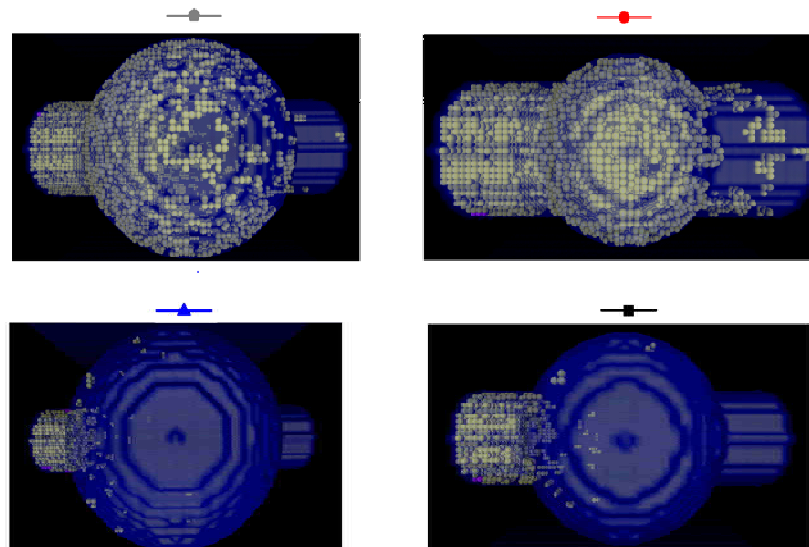
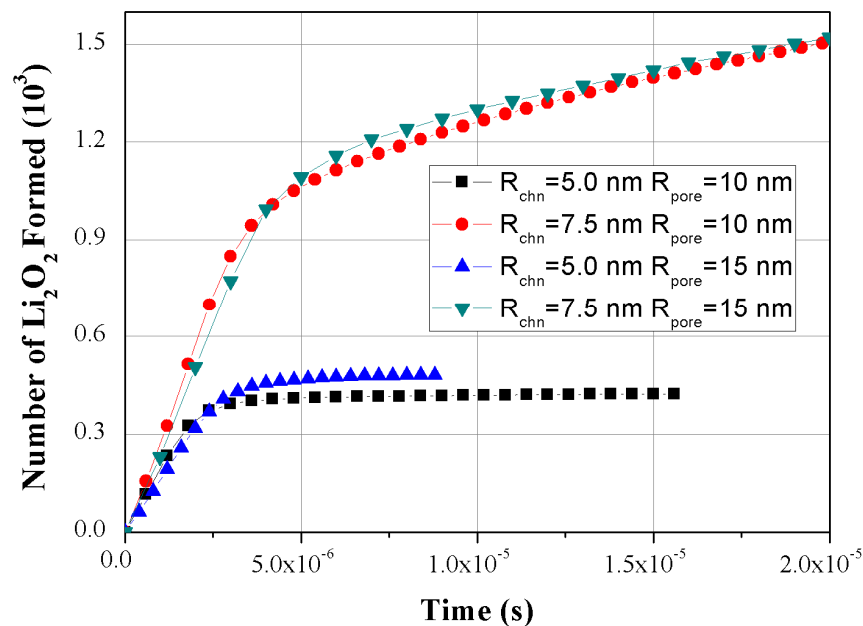


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Mesostructure-performance relationships in batteries...  
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# NANOPORE (3/5): CALCULATED IMPACT OF THE PORE GEOMETRY



Discharge process is limited by channel clogging

Increase the capacity by enlarging the channel size

G. Blanquer, Y. Yin, M.A. Quiroga, A.A. Franco, *J. Electrochem. Soc.*, **163** (3) (2016) A329.

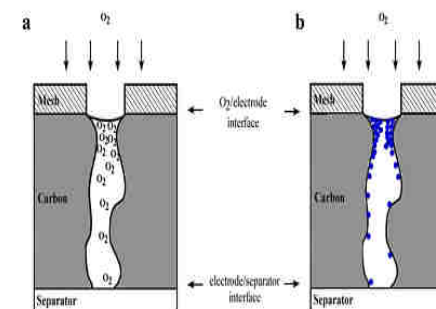
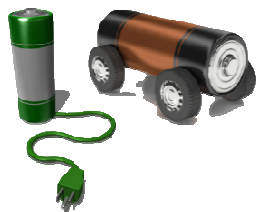


Figure 2. Schematic representation of the oxygen electrode a) before discharge and b) after discharge.

I. Landa-Medrano *et al.*, *J. Electrochem. Soc.*, **162** (2015) A3126.





# NANOPORE (4/5): CALCULATED IMPACT OF THE O<sub>2</sub> DIFFUSION COEFFICIENT

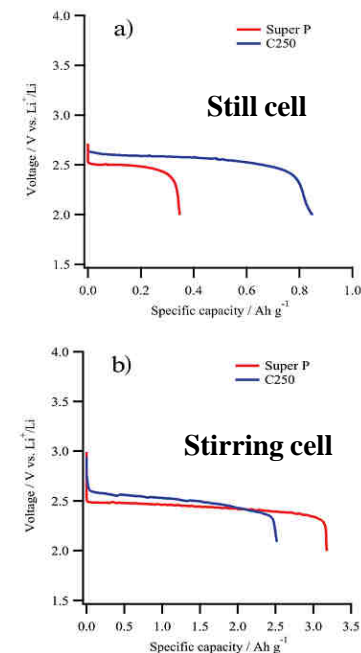
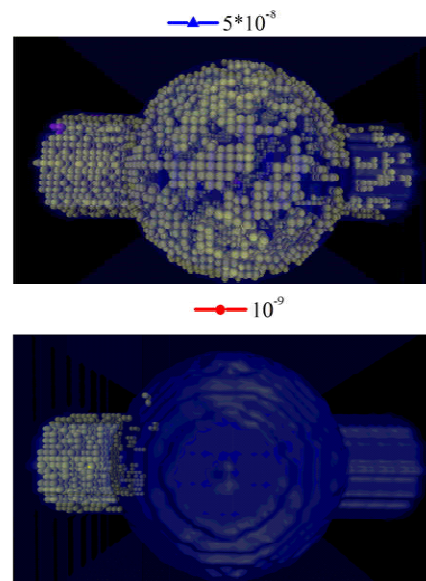
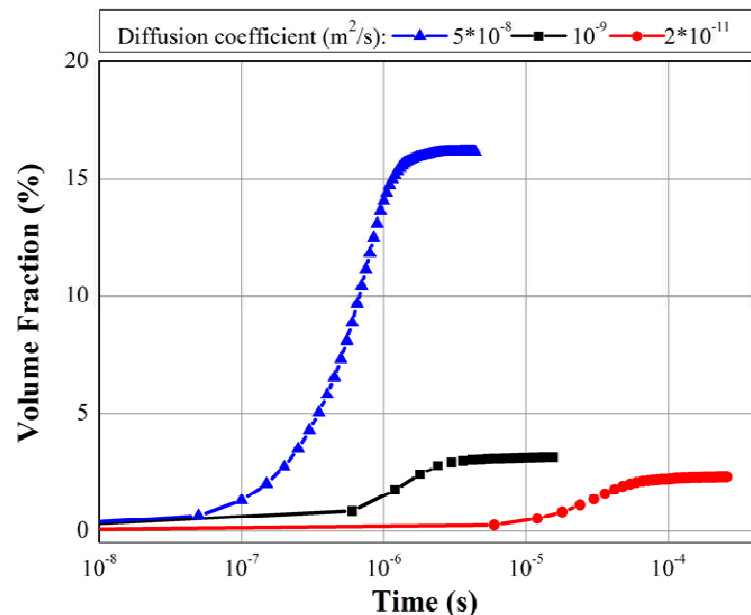


Figure 1. Discharge profiles of Super P and C250 electrodes at 60 °C under a current density of 0.1 mAcm<sup>-2</sup> in a (a) still- and (b) stirred-electrolyte cell.

M. Aklalouch *et al.*, *ChemSusChem*. (2015).

Higher diffusion coefficient  
Higher capacity



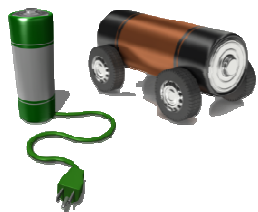
Decrease viscosity of  
electrolyte

G. Blanquer, Y. Yin, M.A. Quiroga, A.A. Franco, *J. Electrochem. Soc.*, **163** (3) (2016) A329.



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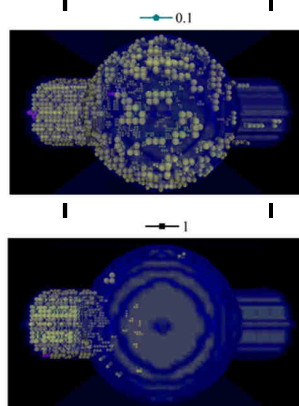
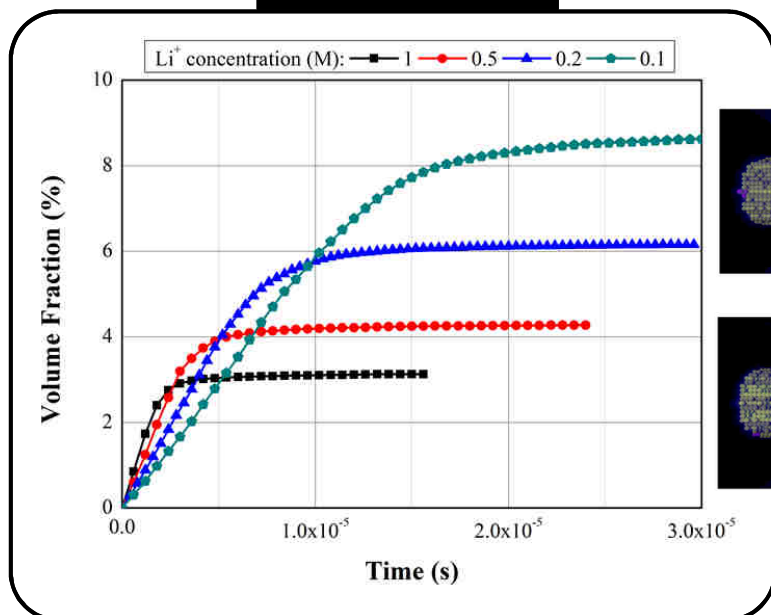




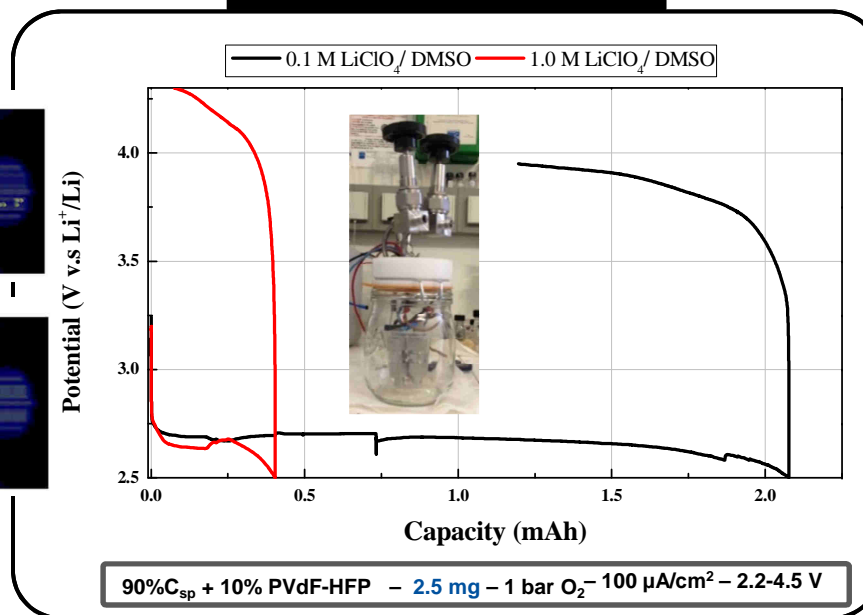
# NANOPORE (5/5): IMPACT OF THE SALT CONCENTRATION ON THE ORR IN PORES

## MODELING

Pore size: 10-30 nm



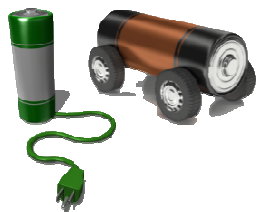
## EXPERIMENTS(\*)



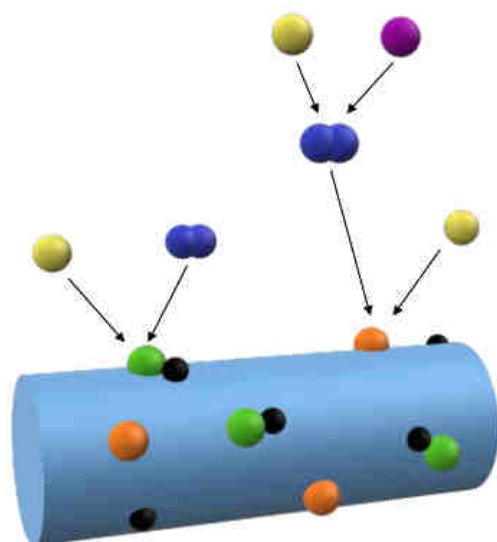
90%C<sub>sp</sub> + 10% PVdF-HFP - 2.5 mg - 1 bar O<sub>2</sub> - 100 μA/cm<sup>2</sup> - 2.2-4.5 V

High Li<sup>+</sup> concentration hinders O<sub>2</sub> transport and accelerates pore clogging.

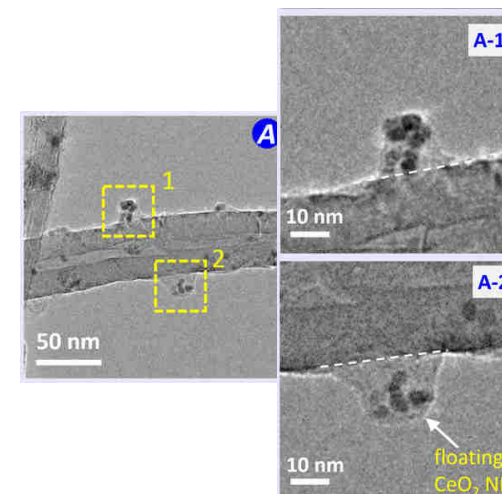
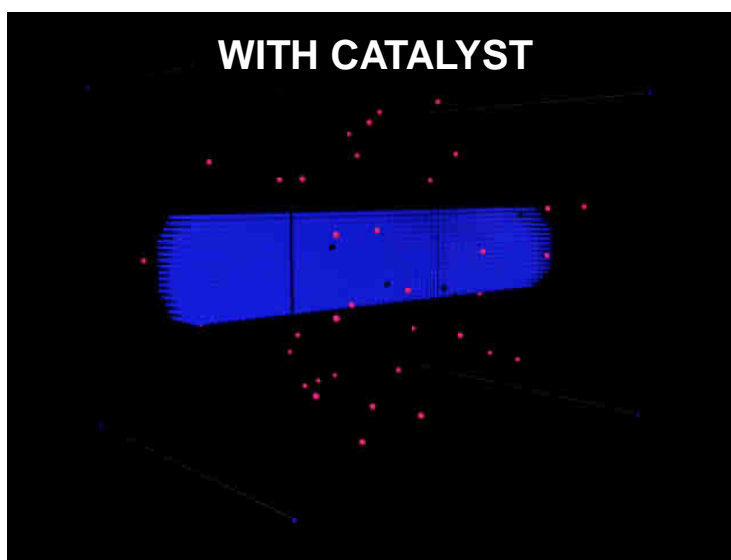
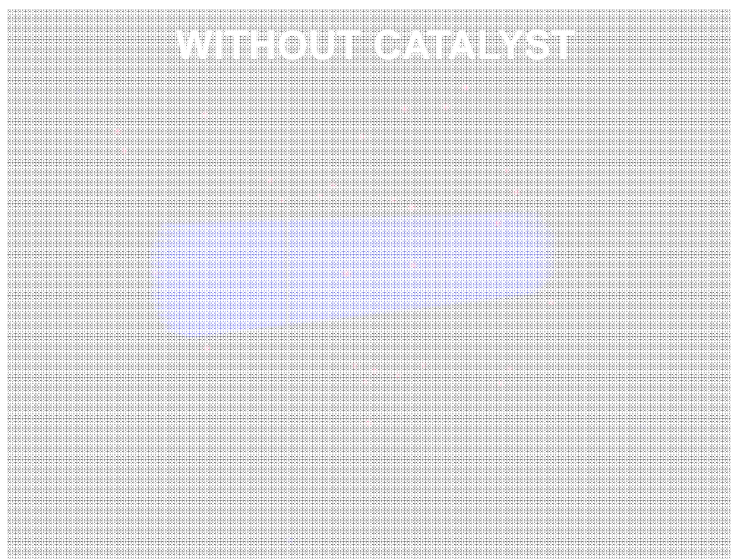
G. Blanquer, Y. Yin, M.A. Quiroga, A.A. Franco, *J. Electrochem. Soc.*, **163** (3) (2016) A329.  
(\*) **Unpublished in house data.** Similar trend also reported in J. Read et al., *J. Electrochem. Soc.*, **150** (2003) A1351.



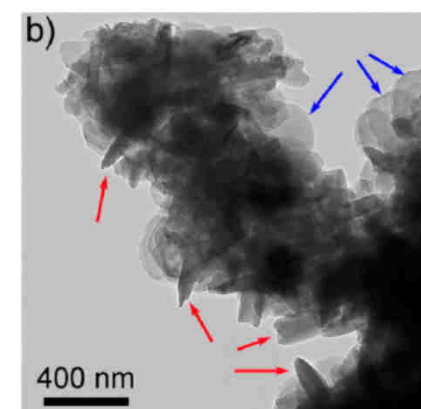
# CARBON FIBER (1/2): IMPACT OF CATALYST ON THE OXYGEN REDUCTION REACTION



- $\text{Li}^+$
- $\text{O}_2$
- $\text{LiO}_2(\text{ip})$
- $\text{Li}_2\text{O}_2$  grown on carbon
- $\text{Li}_2\text{O}_2$  grown on catalyst
- Catalyst

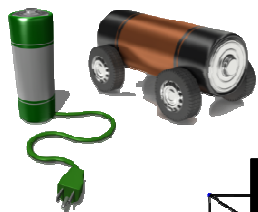


Yang *et al.*, *Nano Lett.*, 16 (2016) 2969.

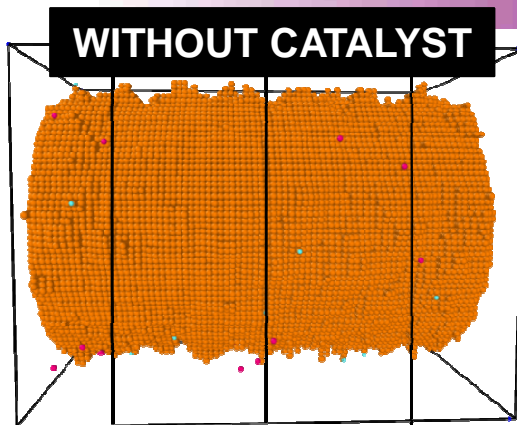


Shui *et al.*, *ACS Nano*, 8 (2014) 3015

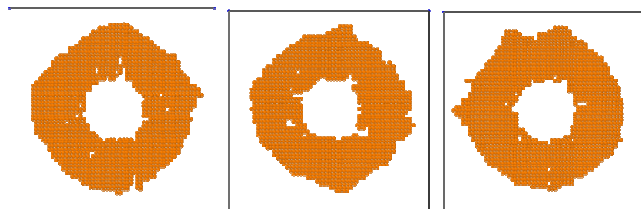
Y. Yin, R. Zhao, Y. Deng, A.A. Franco, *J. Phys. Chem. Letters*, under revision (2016).  
 G. Blanquer, Y. Yin, M.A. Quiroga, A.A. Franco, *J. Electrochem. Soc.*, **163** (3) (2016) A329.



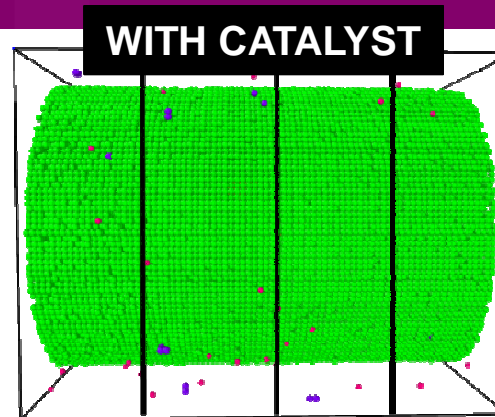
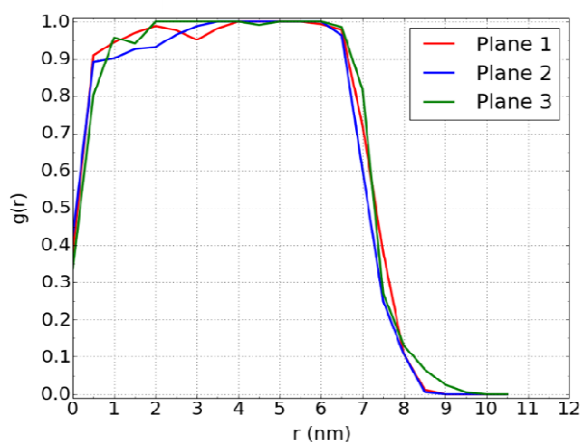
# CARBON FIBER (2/2): IMPACT OF CATALYST ON THE OXYGEN REDUCTION REACTION



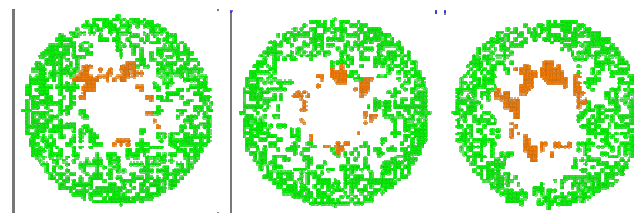
Plane 1 Plane 2 Plane 3



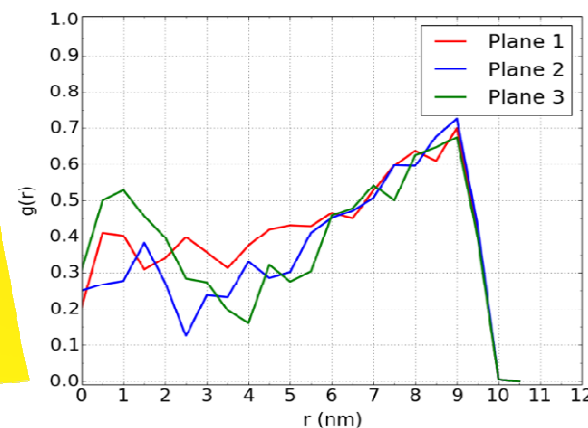
Plane 1 Plane 2 Plane 3



Plane 1 Plane 2 Plane 3

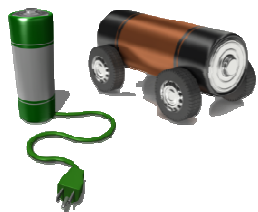


Plane 1 Plane 2 Plane 3



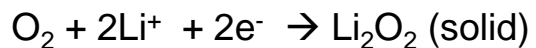
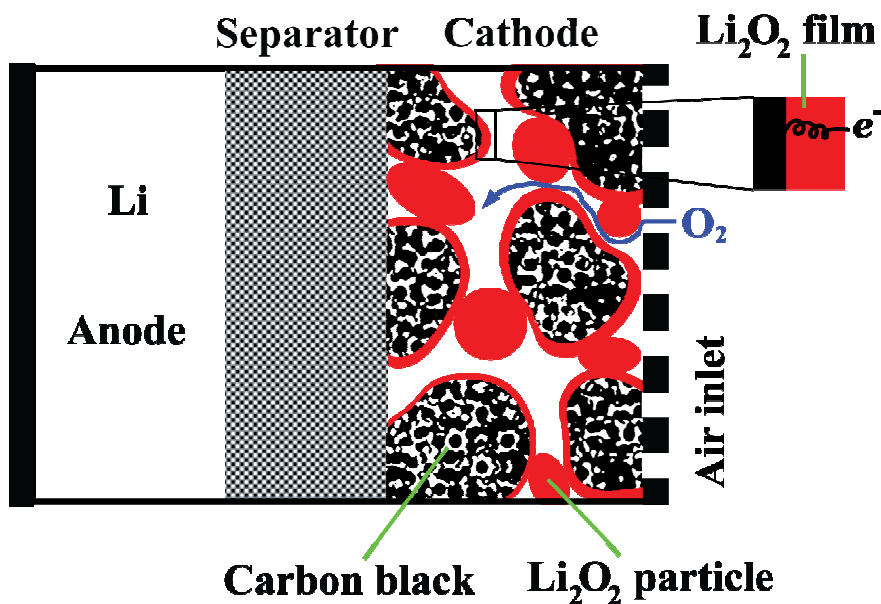
↑ #defects  
↑ porosity

Y. Yin, R. Zhao, Y. Deng, A.A. Franco, *J. Phys. Chem. Letters*, under revision (2016).  
G. Blanquer, Y. Yin, M.A. Quiroga, A.A. Franco, *J. Electrochem. Soc.*, **163** (3) (2016) A329.



# POROUS ELECTRODES IN LITHIUM-O<sub>2</sub> BATTERIES

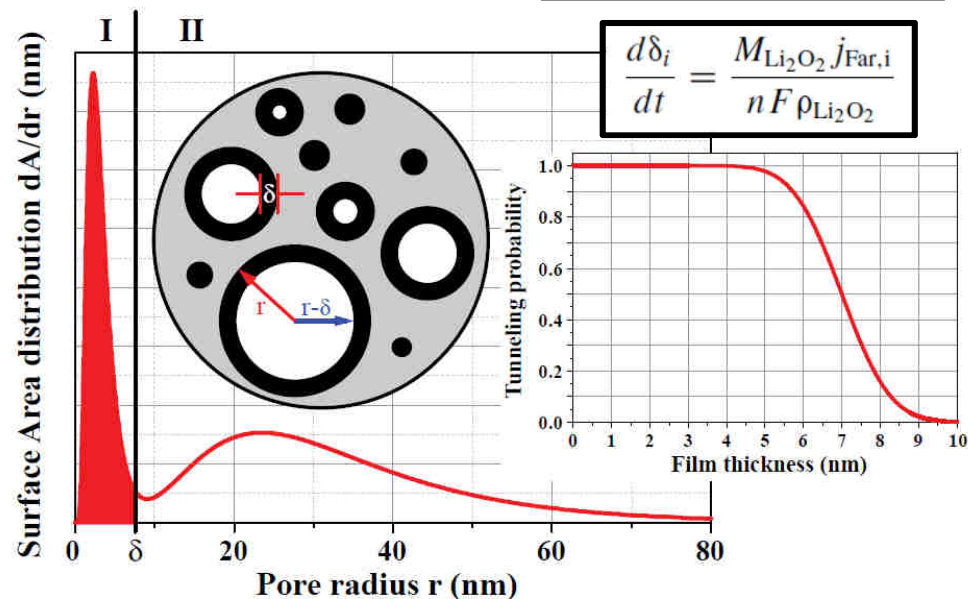
## Lithium O<sub>2</sub> Battery at discharge



## Thin film mechanism

$$a_i = \left[ \frac{1 - \text{erf}(\delta - \gamma)}{2} \right] a_i^0$$

$$\frac{d\delta_i}{dt} = \frac{M_{\text{Li}_2\text{O}_2} j_{\text{Far},i}}{n F \rho_{\text{Li}_2\text{O}_2}}$$



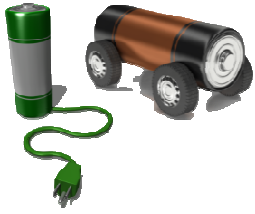
→ Porosity vs. Electronic tunneling probability vs. Reactive surface area.

A.A. Franco, K.H. Xue, *ECS J. Solid State Science and Tech.*, **2** (10) (2013) M3084.  
K.H. Xue, T.K. Nguyen, A.A. Franco, *J. Electrochem. Soc.*, **161** (8) (2014) E3028.



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# CONTINUUM SIMULATION OF SPECIES TRANSPORT @ MACROSCALE

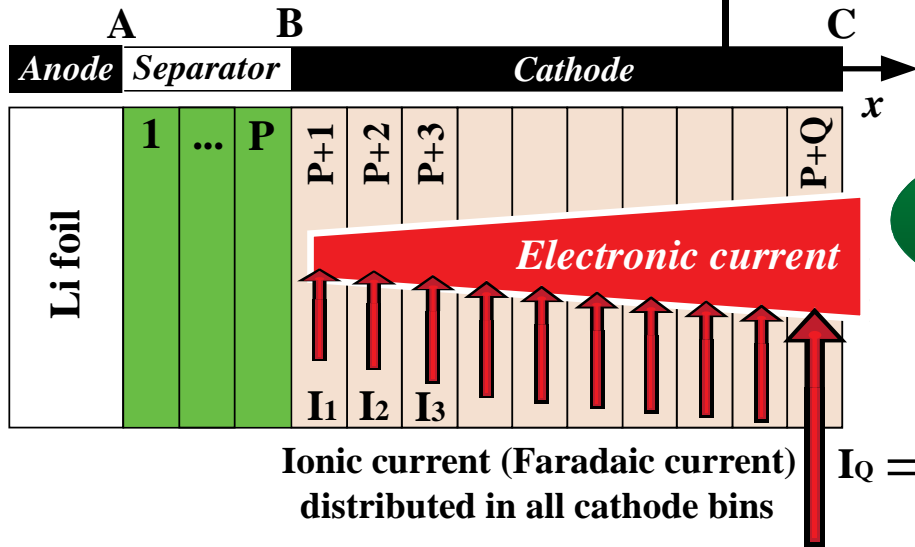
## DIFFUSION EQUATION

$$\frac{\partial(\epsilon C(x,t))}{\partial t} = \frac{\partial}{\partial x} \left( D \frac{\partial C(x,t)}{\partial x} \right) + \gamma \cdot j(x,t)$$

$$D = \left( \frac{\epsilon}{\tau} \right) D_0$$

$$\epsilon = (1 - s) \epsilon_0$$

$$s \approx \int j(x,t) dt$$



Specific surface area (m<sup>2</sup>/m<sup>3</sup>)

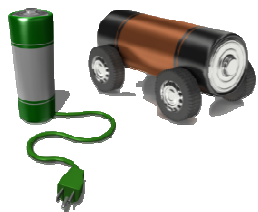
Ionic current (Faradaic current) distributed in all cathode bins

$$I_Q = j(x,t) = f(C_{Li^+}, C_j \dots)$$

Finite Volume Method

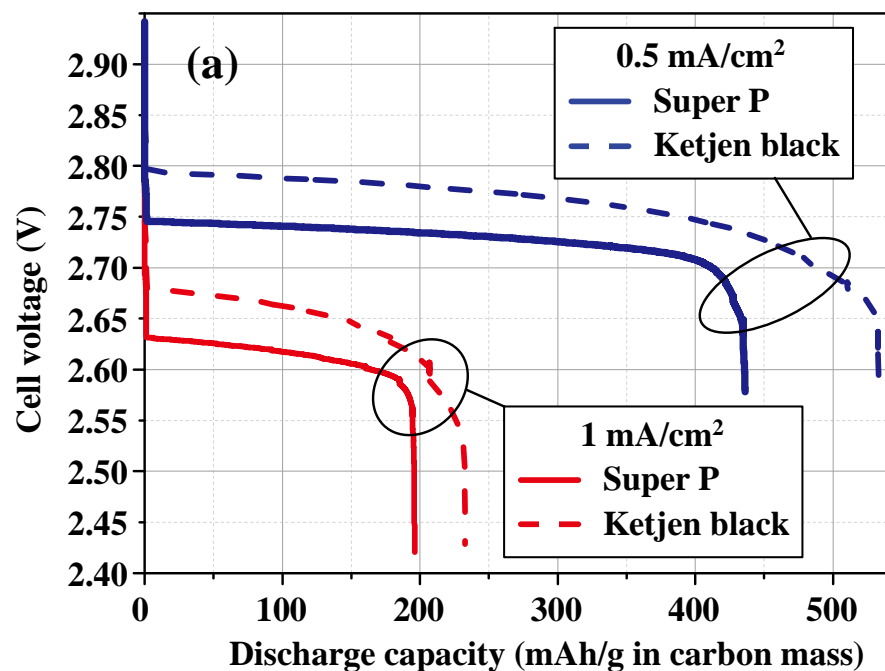
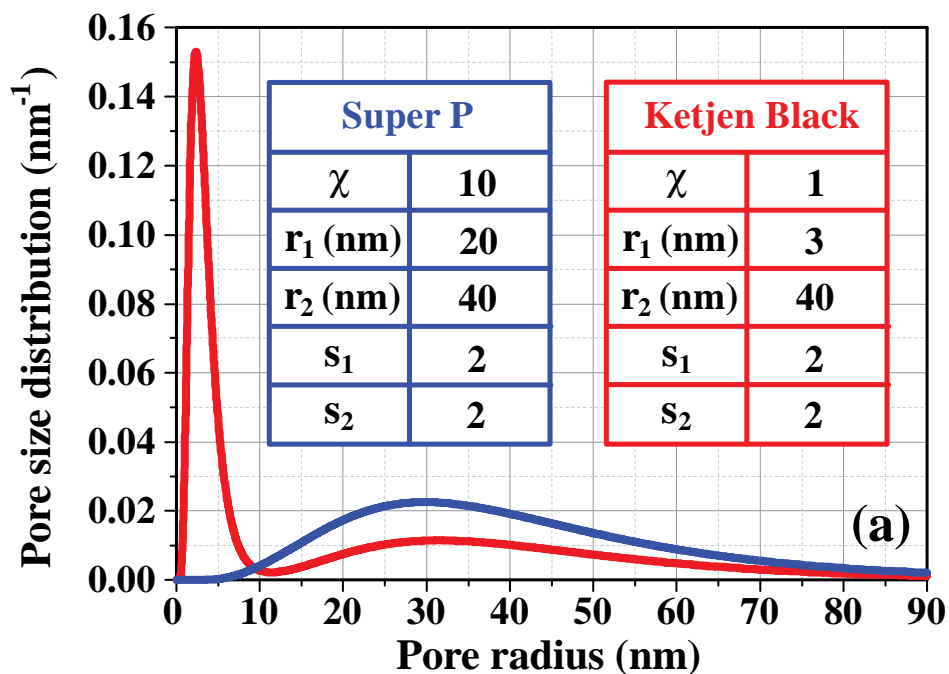
Function calculated by the kinetic model (e.g. KMC or Butler-Volmer)





# IMPACT OF THE PSD ON THE DISCHARGE CURVE

→ For intermediate and high current densities, KB provides lower overpotential and higher capacity than SP.

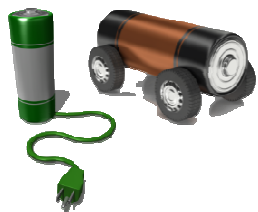


- A.A. Franco, K.H. Xue, *ECS J. Solid State Science and Tech.*, **2** (10) (2013) M3084.
- K.H. Xue, T.K. Nguyen, A.A. Franco, *J. Electrochem. Soc.*, **161** (8) (2014) E3028.



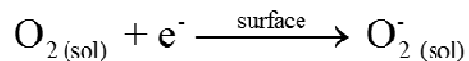
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 Mesostructure-performance relationships in batteries...  
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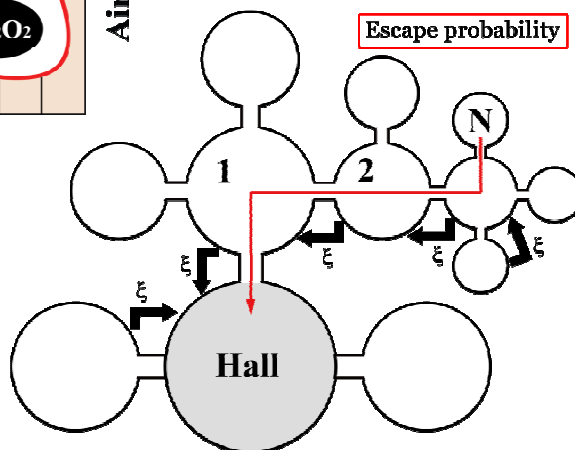
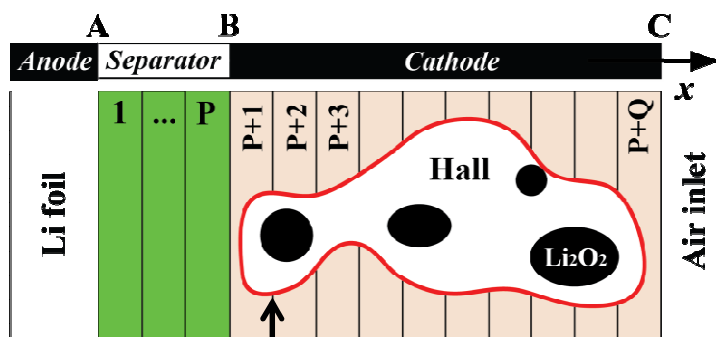
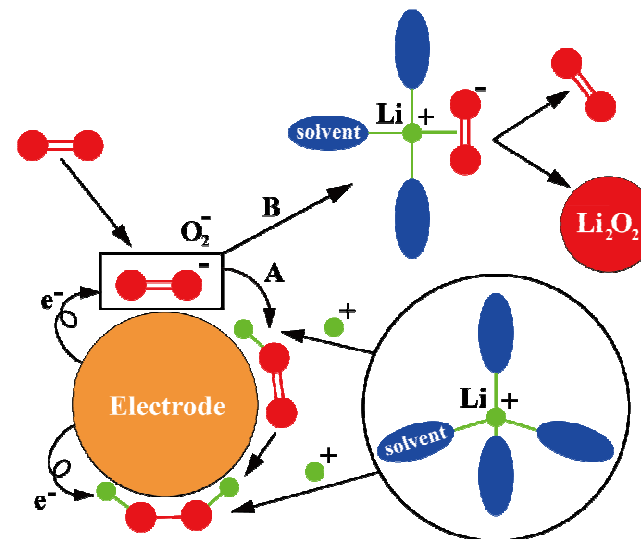
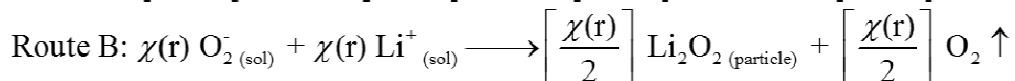
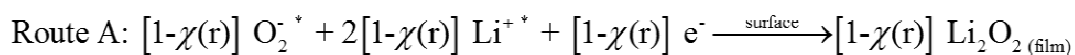
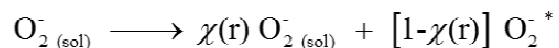


# SOLUTION PHASE: $O_2^-$ ESCAPE PROBABILITY

## First reduction



## Second reduction

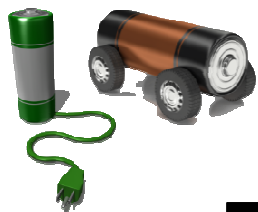


## Escape function

$$\chi(r) = \xi^N = \xi^{\frac{r_{max}-r}{r_{max}}}$$

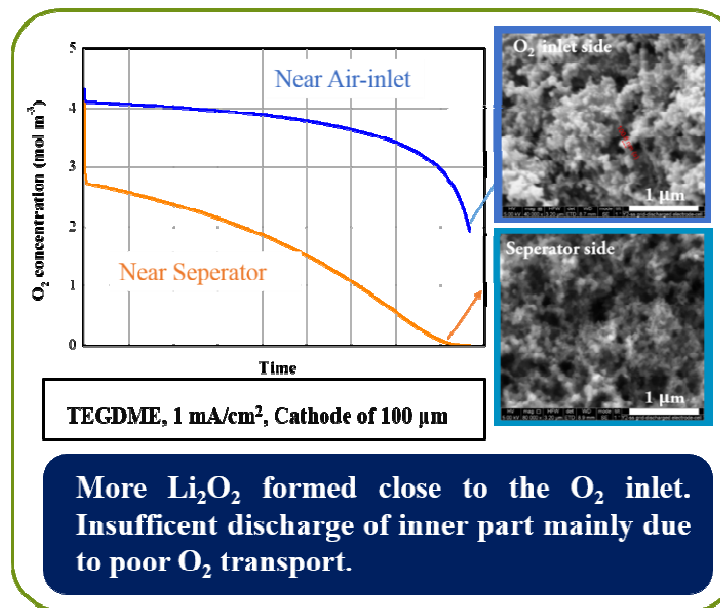
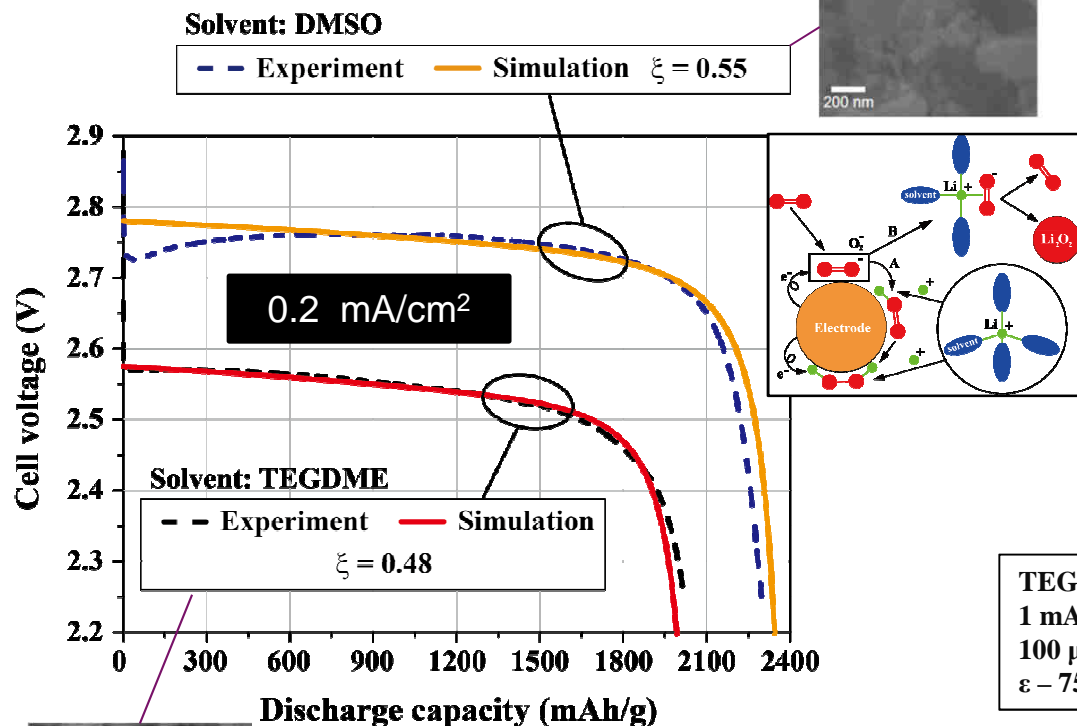
$\xi$  increases with the donor number



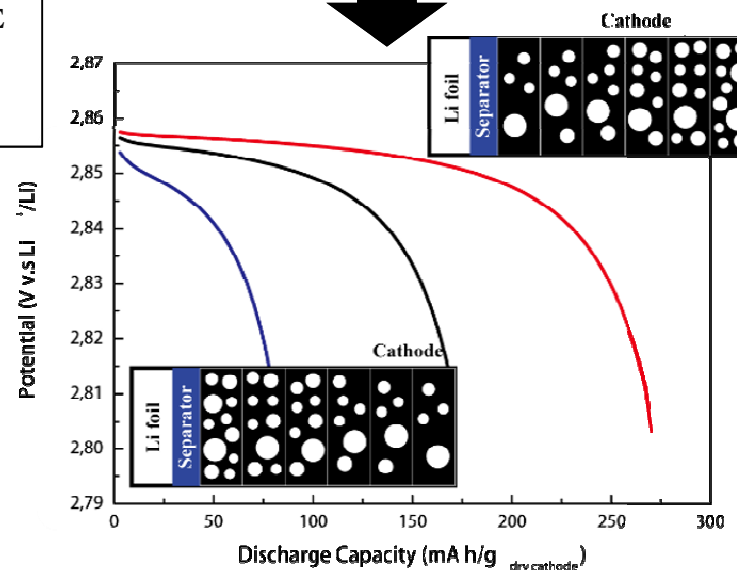


# SOLVENT & ARCHITECTURE IMPACTS ON DISCHARGE

## Impact of solvent



**TEGDME**  
 1 mA/cm<sup>2</sup>  
 100  $\mu$ m  
 $\epsilon = 75\%$



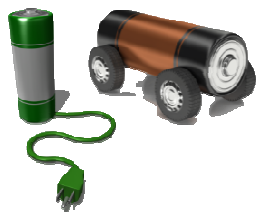
- K.H. Xue, T.K. Nguyen, A.A. Franco, *J. Electrochem. Soc.*, **161** (8) (2014) E3028.
- K.-H. Xue, E. McTurk, L. Johnson, P. G. Bruce, A. A. Franco, *J. Electrochem. Soc.*, **162** (4) (2015) A614 .
- SEM images from: L. Johnson *et al.*, *Nature Chemistry* **6** (2014) 1091

**Li<sub>2</sub>O<sub>2</sub> toroid**



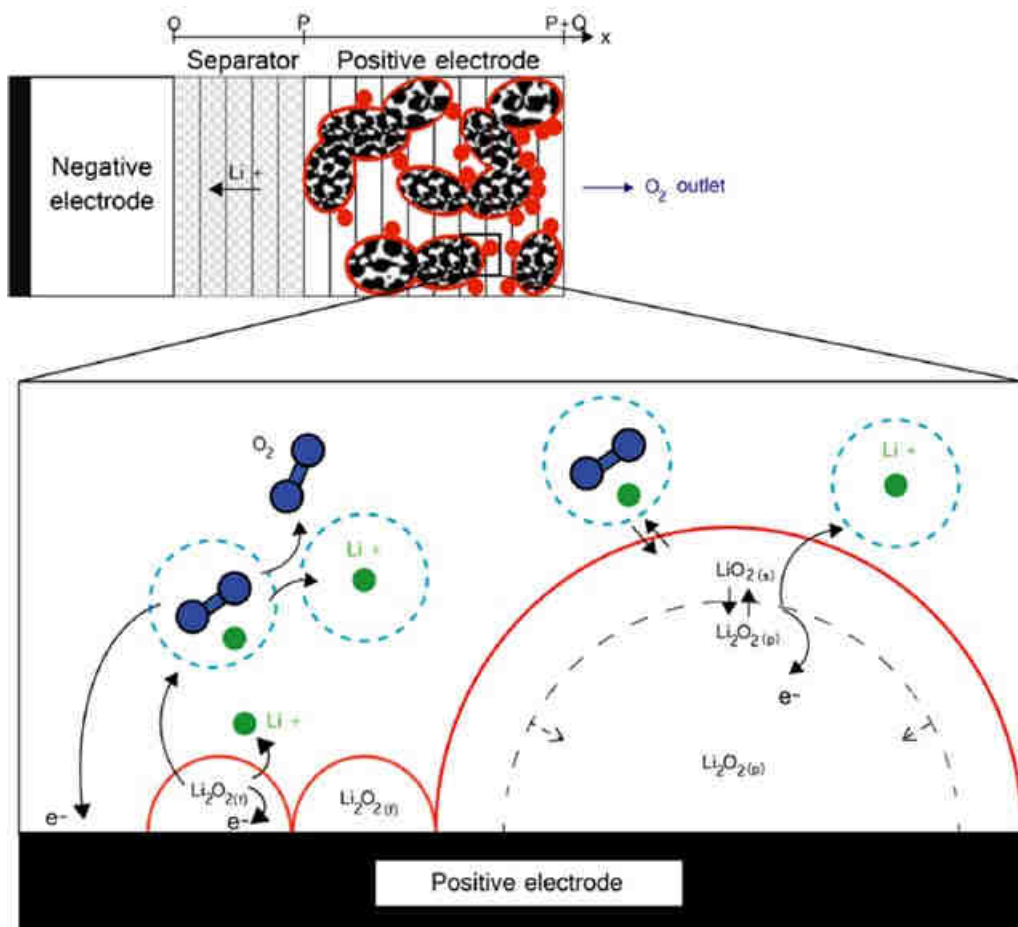
**IMPACT ON CHARGE?**



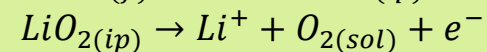
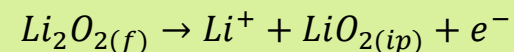


# IMPACT OF DISCHARGE PRODUCTS MORPHOLOGY ON THE CHARGE PROCESS (1/2)

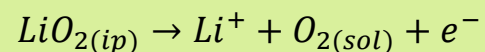
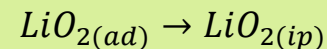
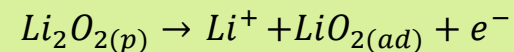
Y. Yin, C. Gaya, A. Torayev, V. Thangavel, A.A. Franco, *The Journal of Physical Chemistry Letters*, 7(19) (2016) 3897.



## Oxidation of Thin-film



## Oxidation of Large-particle

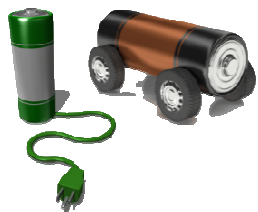


→ Extension of the cell model for charge: capturing impact of  $Li_2O_2$  particle size distribution on charge kinetics.



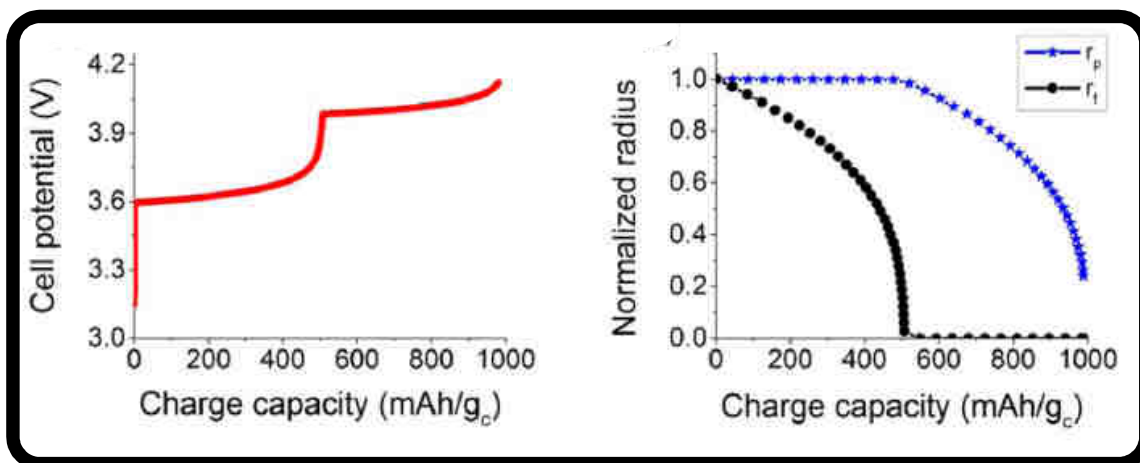
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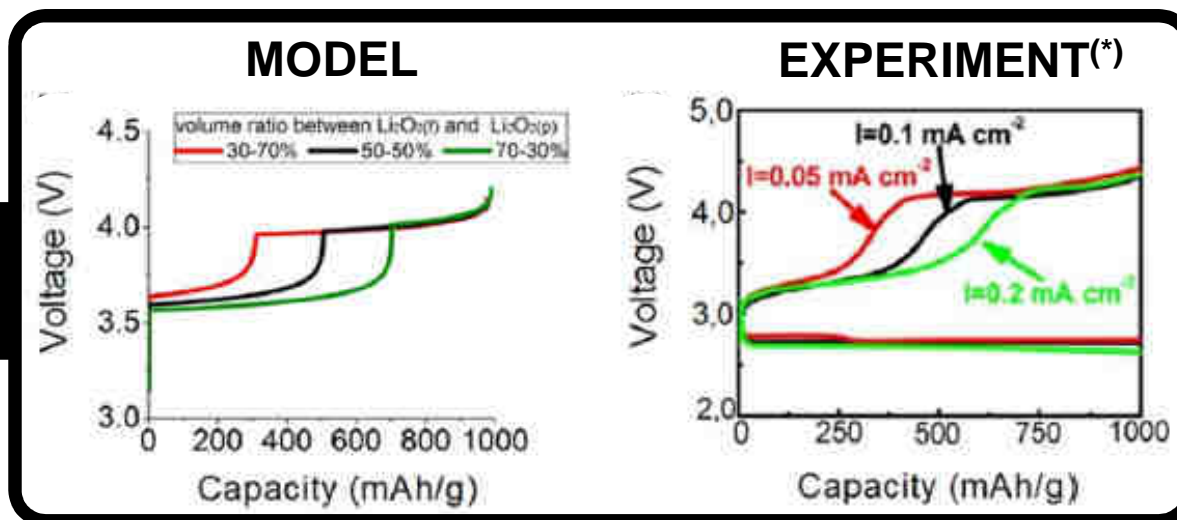
# IMPACT OF DISCHARGE PRODUCTS MORPHOLOGY ON THE CHARGE PROCESS (2/2)

Y. Yin, C. Gaya, A. Torayev, V. Thangavel, A.A. Franco, *The Journal of Physical Chemistry Letters*, 7(19) (2016) 3897.

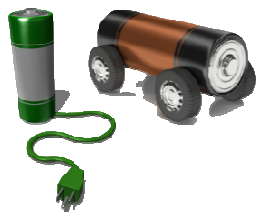


→ Two potential plateaus calculated: linked to the two size of particles consumption.

→ Impact of discharge current density on the charge potential: good agreement with experiment.

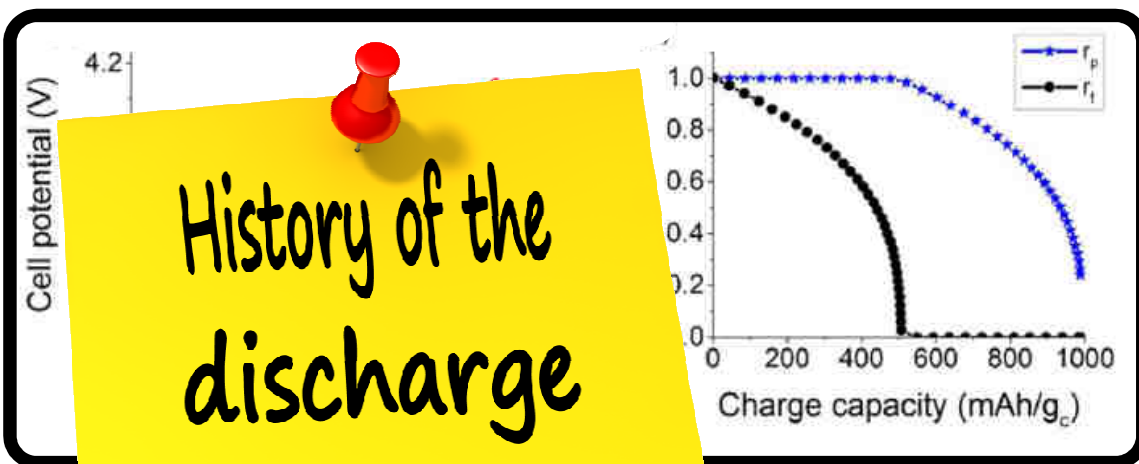


(\*) D. Zhai, H. Wang, J. Yang, K.C. Lau, K. Li, K. Amine, L.A. Curtiss, *J. Am. Chem. Soc.* **135** (2013) 15364.



# IMPACT OF DISCHARGE PRODUCTS MORPHOLOGY ON THE CHARGE PROCESS (2/2)

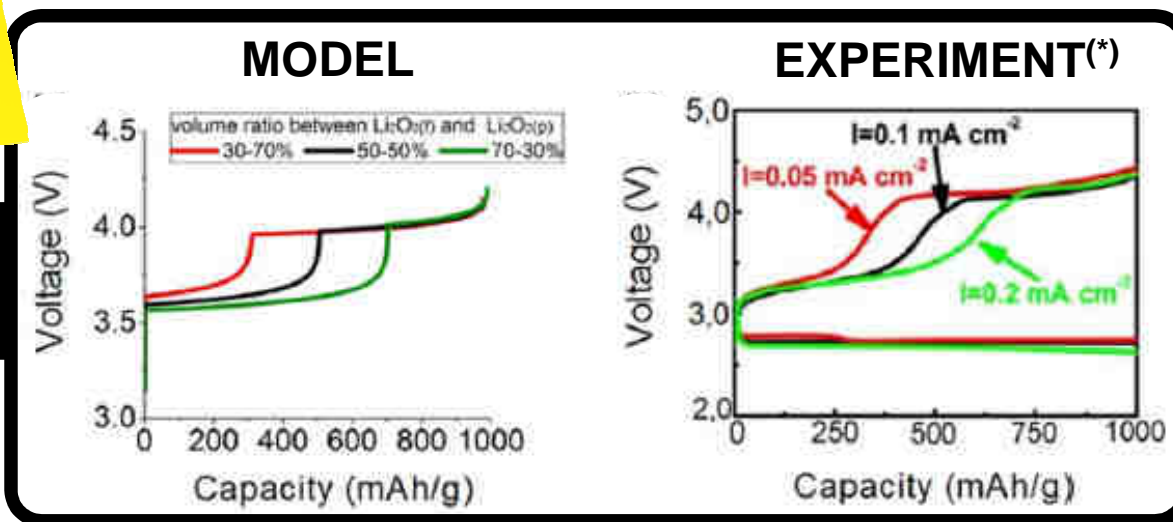
Y. Yin, C. Gaya, A. Torayev, V. Thangavel, A.A. Franco, *The Journal of Physical Chemistry Letters*, 7(19) (2016) 3897.



→ Two potential plateaus calculated: linked to the two size of particles consumption.

History of the discharge impacts charge

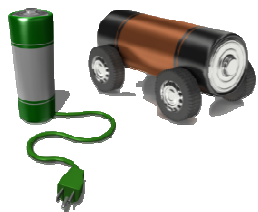
→ Impact of discharge current density on the charge potential: good agreement with experiment.



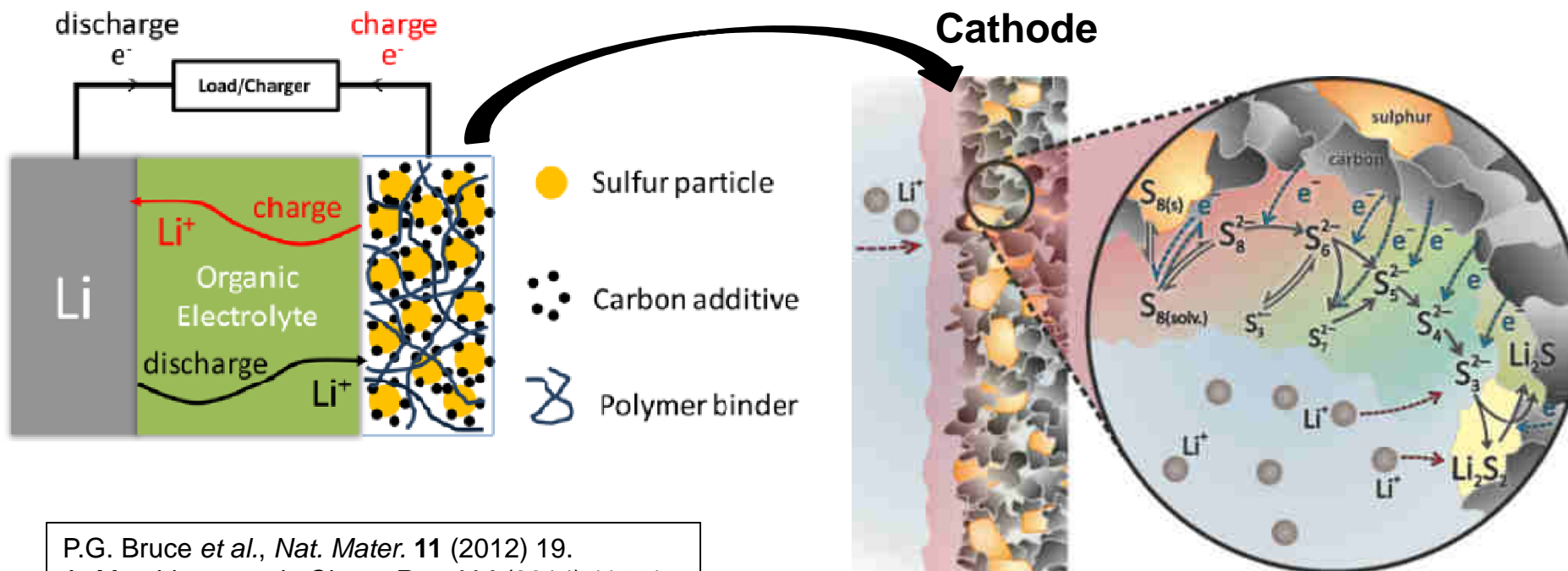
(\*) D. Zhai, H. Wang, J. Yang, K.C. Lau, K. Li, K. Amine, L.A. Curtiss, *J. Am. Chem. Soc.* **135** (2013) 15364.

## 2. LITHIUM-S BATTERIES



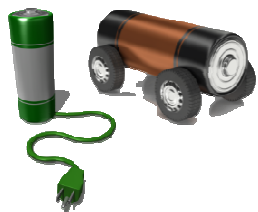


# LITHIUM-SULFUR BATTERIES: MOTIVATION

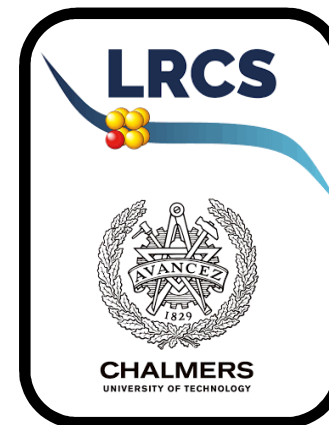
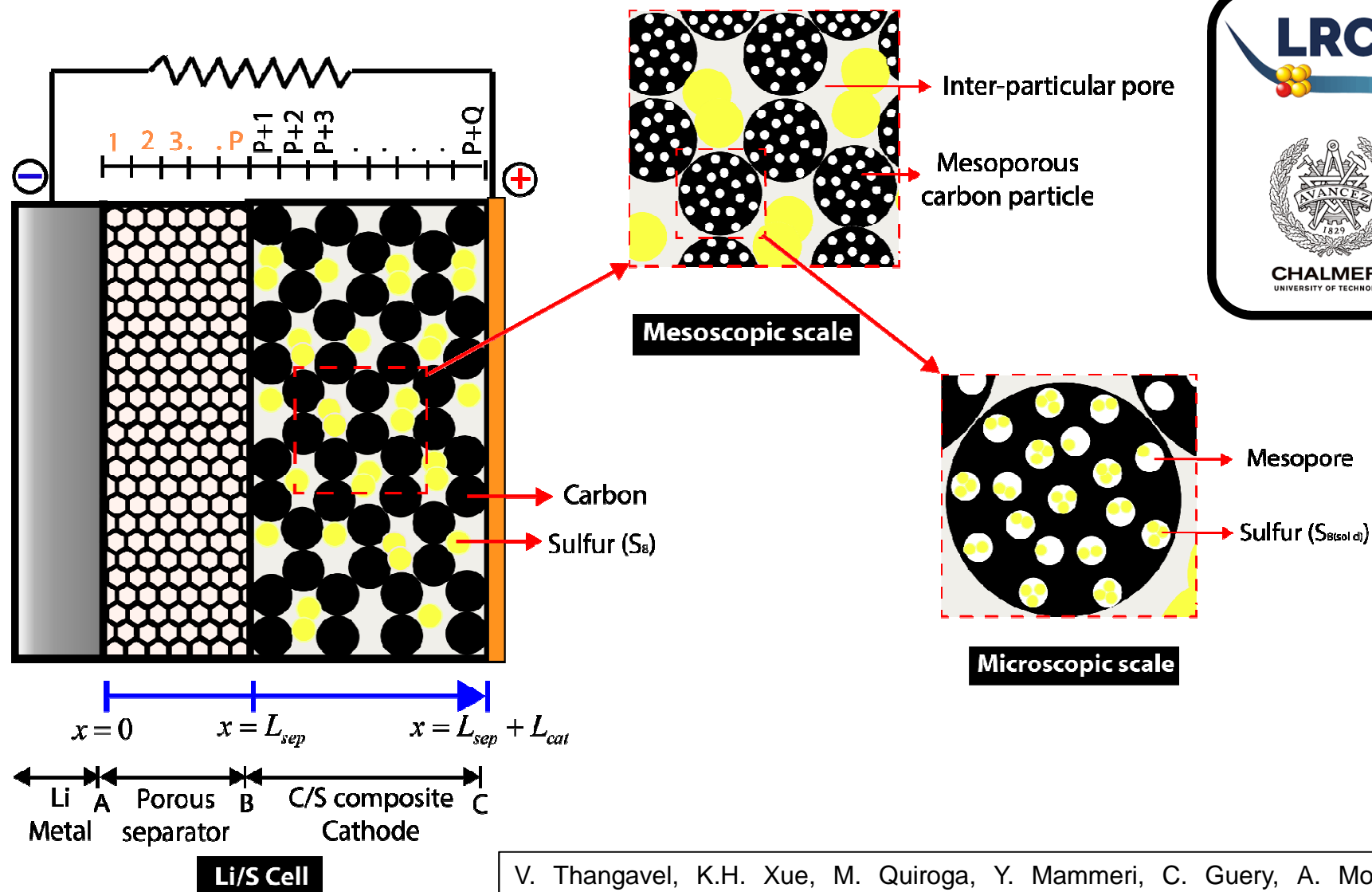


P.G. Bruce *et al.*, *Nat. Mater.* **11** (2012) 19.  
 A. Manthiram *et al.*, *Chem. Rev.* **114** (2014) 11751.

→ **Key to enhance LiS batteries:** deeper insights about the electrolyte composition and porous electrode microstructure impact on the cell performance.  
 ↳ e.g. sulfur repartition between different scales of porosity,  $Li_2S$  location...

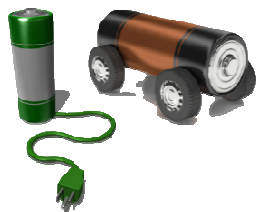


# 1D-CONTINUUM CELL MODEL

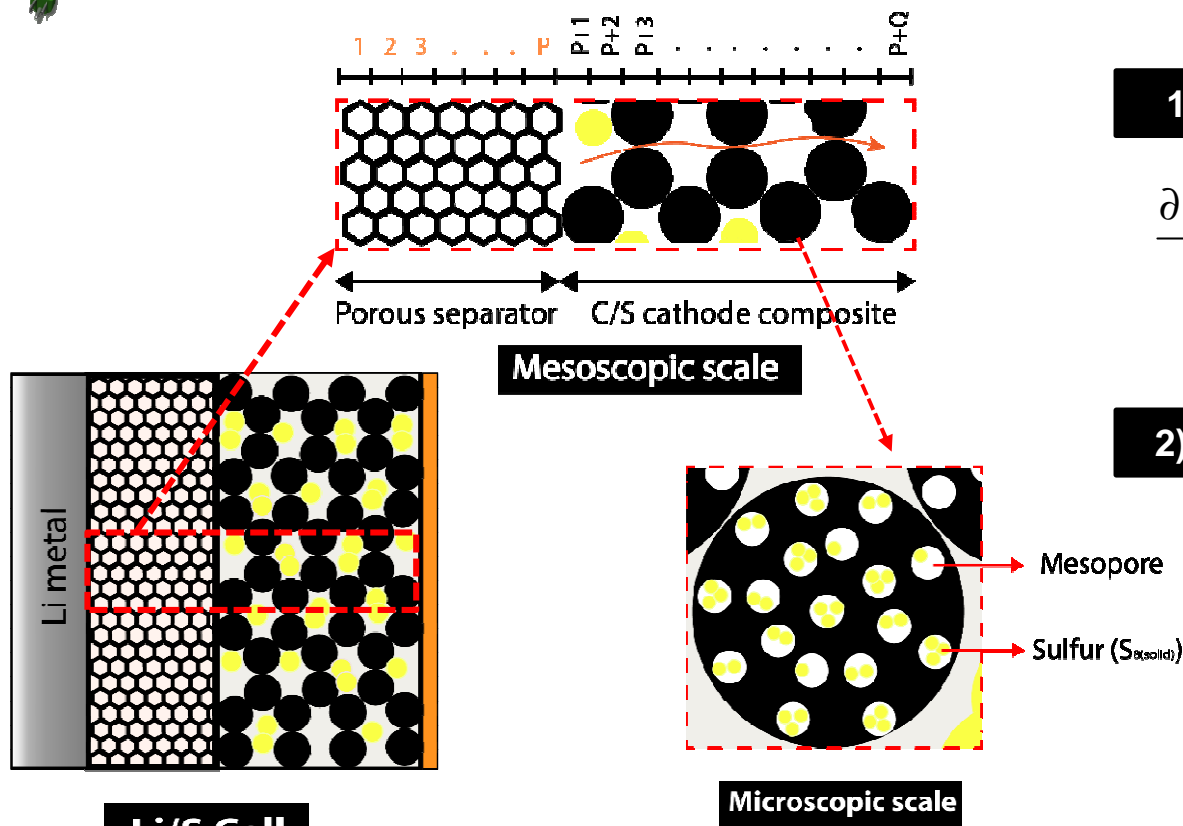


V. Thangavel, K.H. Xue, M. Quiroga, Y. Mammeri, C. Guery, A. Moustari, P. Johansson, M. Morcrette, A.A. Franco, **163** (13) (2016) A2817.





# SULFUR-BASED SPECIES TRANSPORT



## 1) Mass conservation for mesoscale

$$\frac{\partial(\epsilon_1 c_1)}{\partial t} = \frac{\partial}{\partial x} \left[ (\epsilon_1)^{1.5} D \left( \frac{\partial c_1}{\partial x} \right) \right] + r_1 - R_1 + f$$

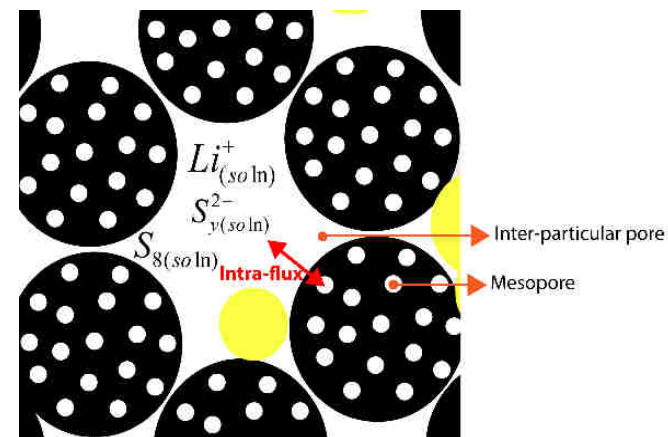
## 2) Mass conservation for microscale

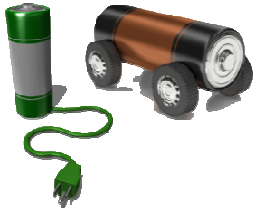
$$\frac{\partial(\epsilon_2 c_2)}{\partial t} = r_2 - R_2 - f$$

## 3) Intra-flux between two scales

$$f \propto K_{flux} (c_2 - c_1) \Xi(\delta_1)$$

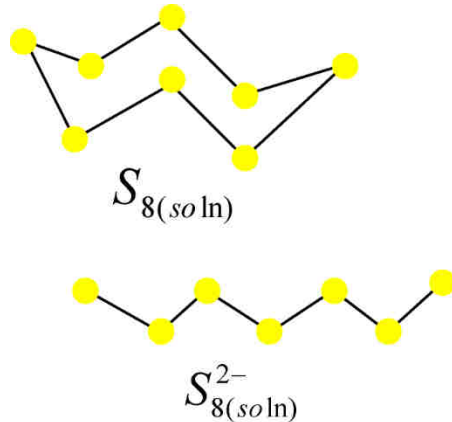
$r$ : generation rate through electrochemical reactions  
 $R$ : sink rate due to chemical dissolution/precipitation  
 $f$ : species intra-flux between the two scales





# SULFUR-BASED SPECIES TRANSPORT

↳ During the initial stage of discharge long chain polysulfides are produced which can increase the viscosity of the electrolyte.



↳ Diffusion coefficient is inversely proportional to viscosity according to Stokes-Einstein equation.

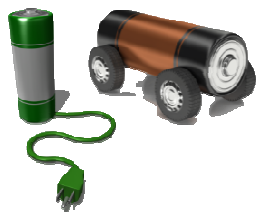
$$D \propto \frac{1}{\mu}$$

↳ Viscosity of the electrolyte can be determined from Einstein's theory of suspension.

$$\frac{\mu}{\mu_0} = \frac{1+0.5\varphi}{(1-\varphi)^4}$$

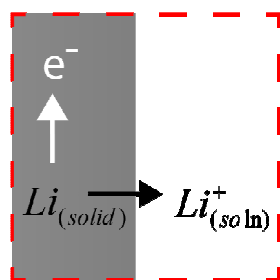
$\mu_0$ : Viscosity of the pure electrolyte.  
 $\varphi$ : Volume fraction of long chain polysulfides.  
 $\bar{V}_{S_8}, \bar{V}_{S_8^{2-}}$ : Partial molar volume of  $S_8$  and  $S_8^{2-}$

$$\varphi = c_1 (S_8) \bar{V}_{S_8} + c_1 (S_8^{2-}) \bar{V}_{S_8^{2-}}$$

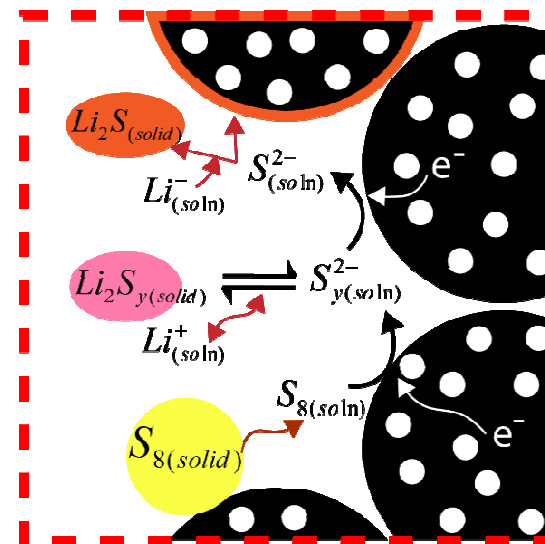


# ELECTROCHEMICAL & PRECIPITATION REACTIONS

↳ The dissolved sulfur ( $S_{8(soln)}$ ) undergoes a series of elementary reduction reactions to produce  $S_{(soln)}^{2-}$ .



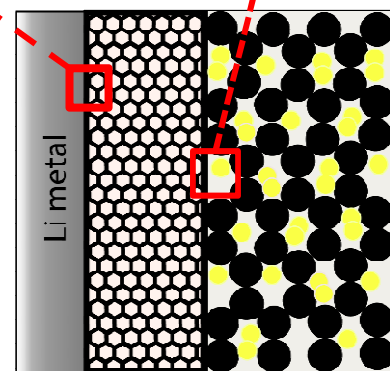
**Anode side**



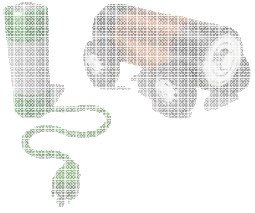
**Cathode side**

y: 8, 6, 4 & 2

- ↳ Precipitation/dissolution of  $Li_2S_y_{(solid)}$ .
- ↳  $Li_2S$  precipitates both as film and particle.



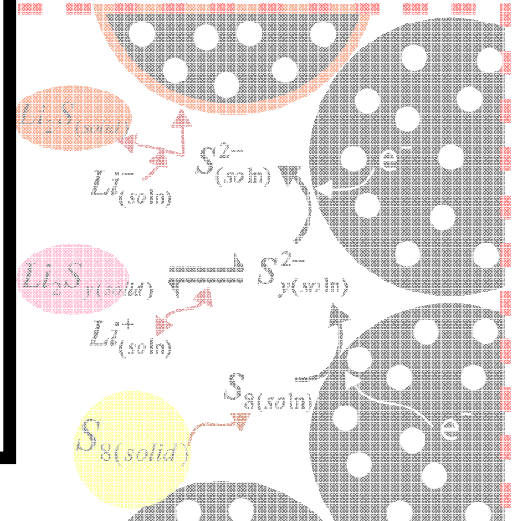
**L** /: mesoscale or microscale.



# ELECTROCHEMICAL & PRECIPITATION REACTIONS

↳ The dissolved sulfur elementary reduction

$$\frac{\partial \varepsilon^l}{\partial t} \propto - \sum_k \nu_i^l$$

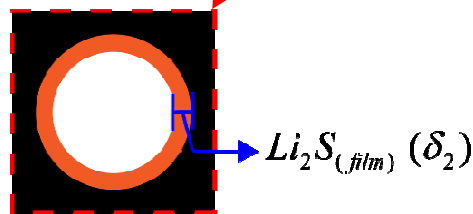
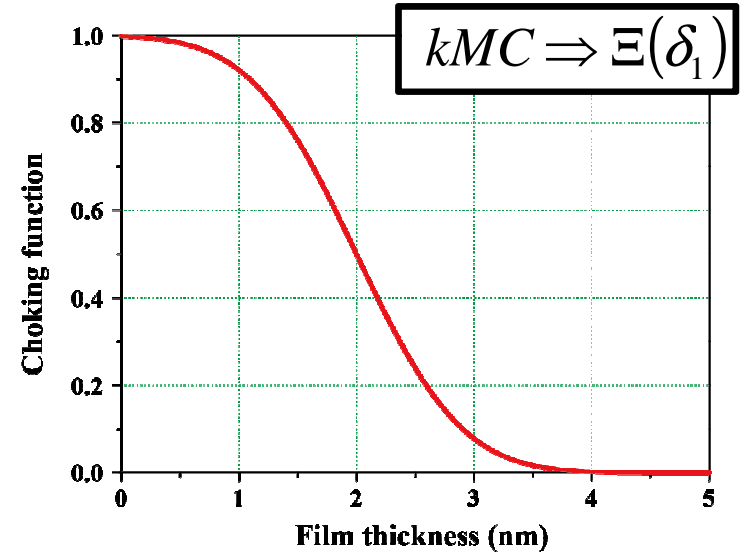
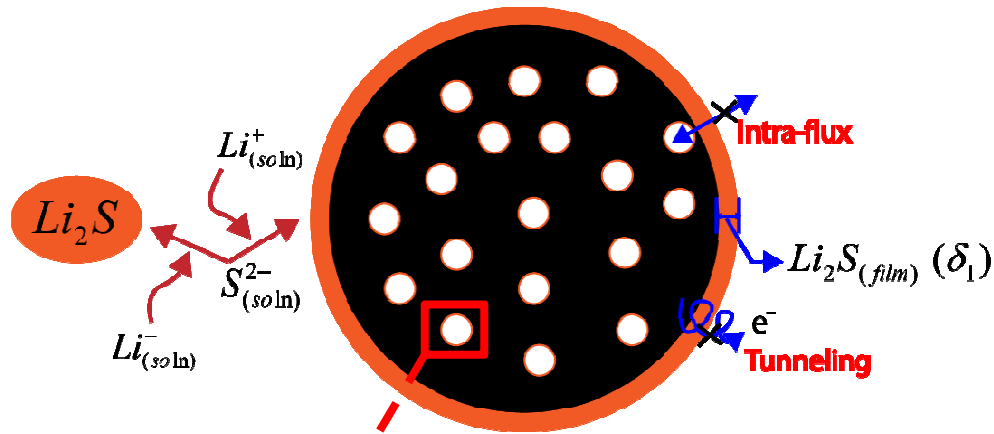


$$\nu_i^l \propto a^l(t) \left( k_i \prod_j C_j^l - k_{-i} \prod_{j'} C_{j'}^l \right)$$

$l$ : mesoscale or microscale.



# ACTIVE SURFACE AREA LOSS

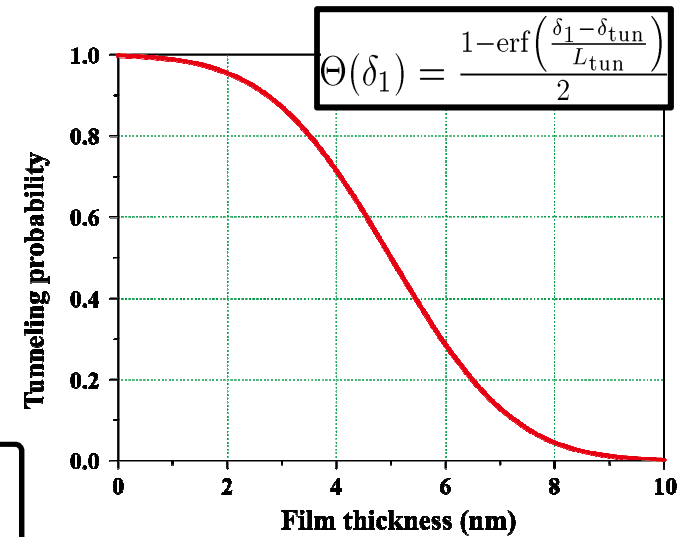


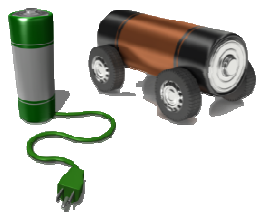
## Active surface area evolution

$$a_1 = a_1^{\max} \left[ 1 - \frac{e_{k1}(S_8)}{\epsilon_1^{\max}} \right]^{1.5} \Theta(\delta_1)$$

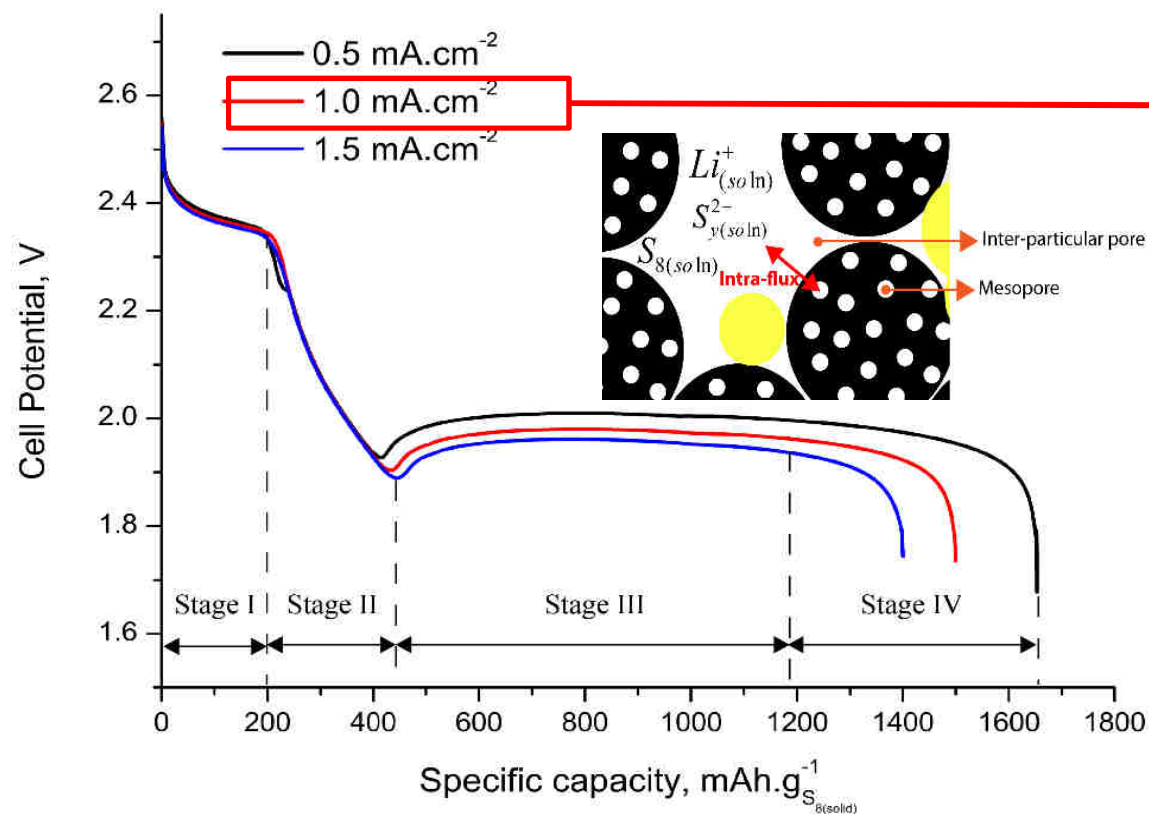
$$a_2 = a_2^{\max} \left( \frac{R_p - \delta_2}{R_p} \right)^2 \Theta(\delta_2) \Xi(\delta_1)$$

$\delta_1, \delta_2$  :  $\text{Li}_2\text{S}$  thin film thickness over the surface of carbon  
 $\delta_{\text{tun}}$  : tunneling threshold

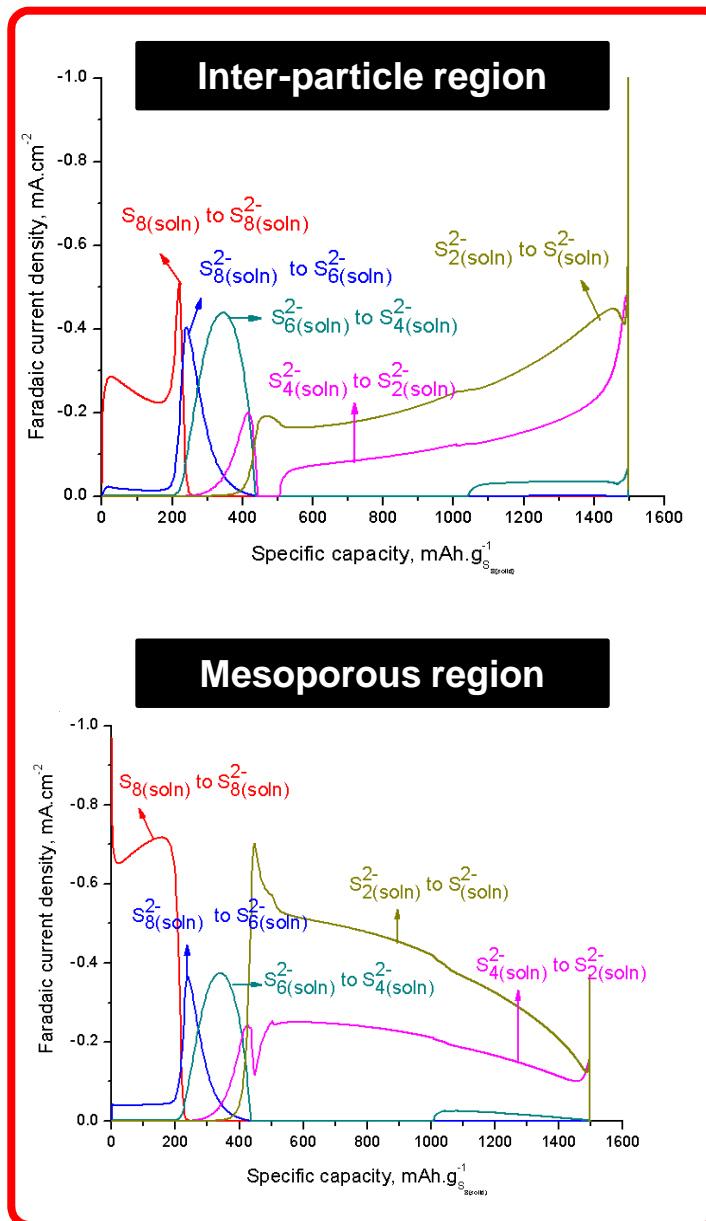




# HETEROGENEITY OF REACTIONS AT MULTIPLE PORE SCALES



V. Thangavel, K.H. Xue, M. Quiroga, Y. Mammeri, C. Guery, A. Moustari, P. Johansson, M. Morcrette, A.A. Franco, **163** (13) (2016) A2817.

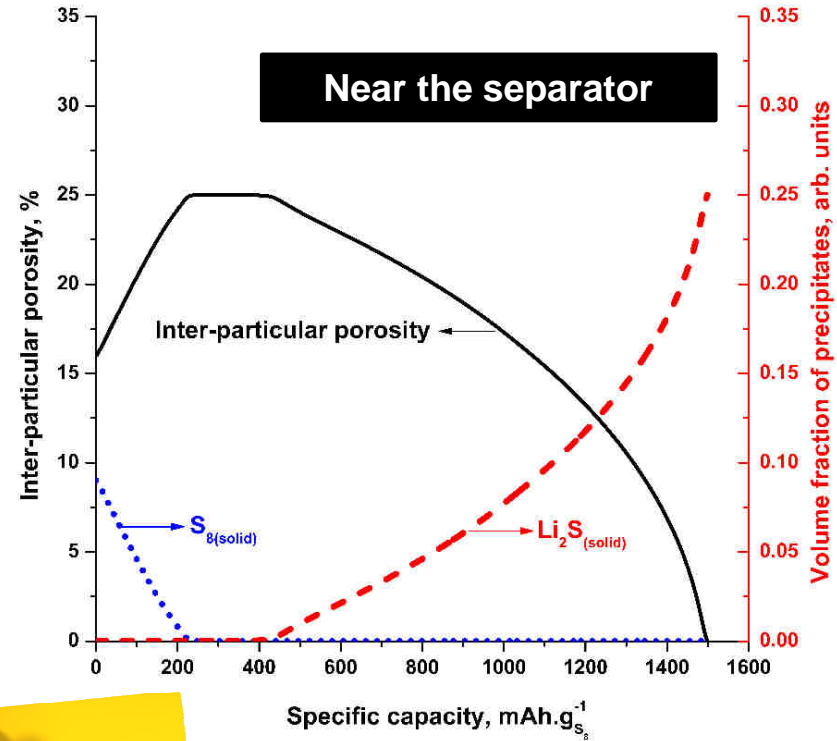
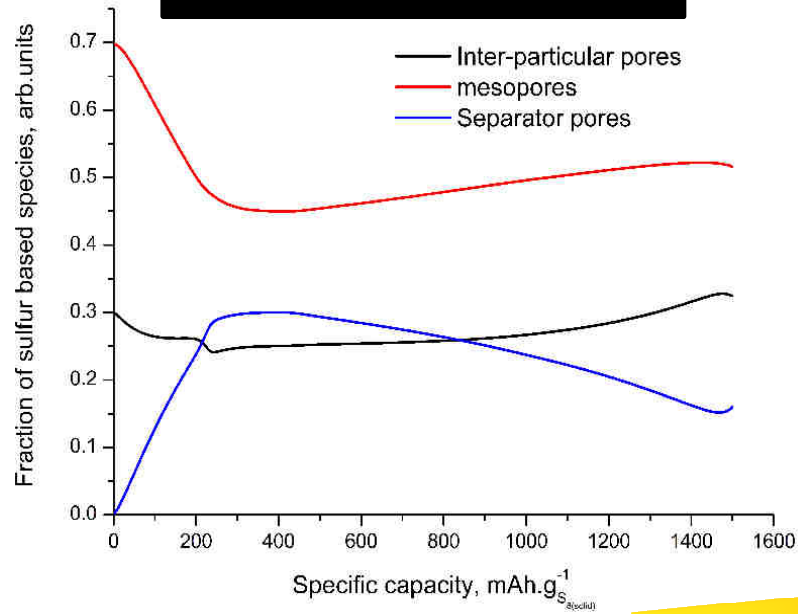




# HETEROGENEITY OF REACTIONS ALONG THE CATHODE THICKNESS (1/2)

1.0 mA.cm<sup>-2</sup>

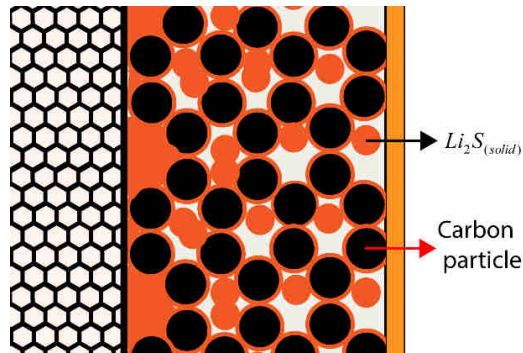
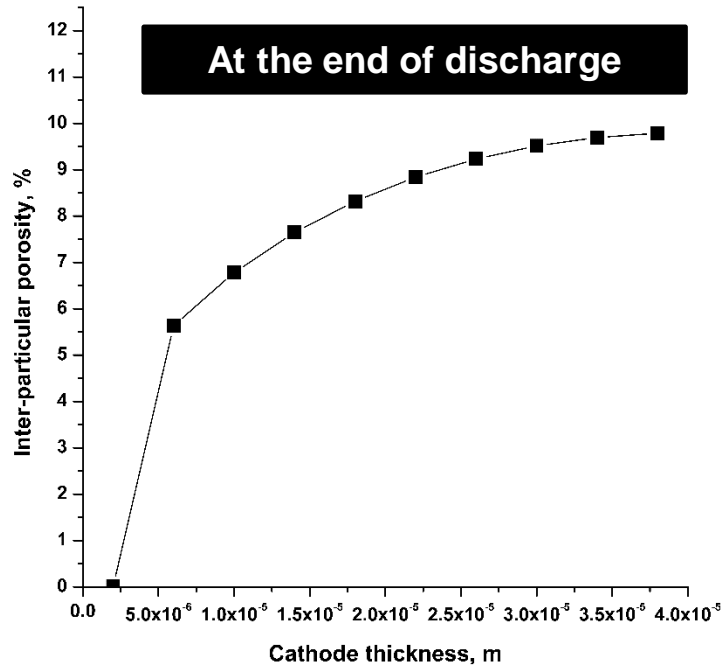
Exchange of sulfur between various domains



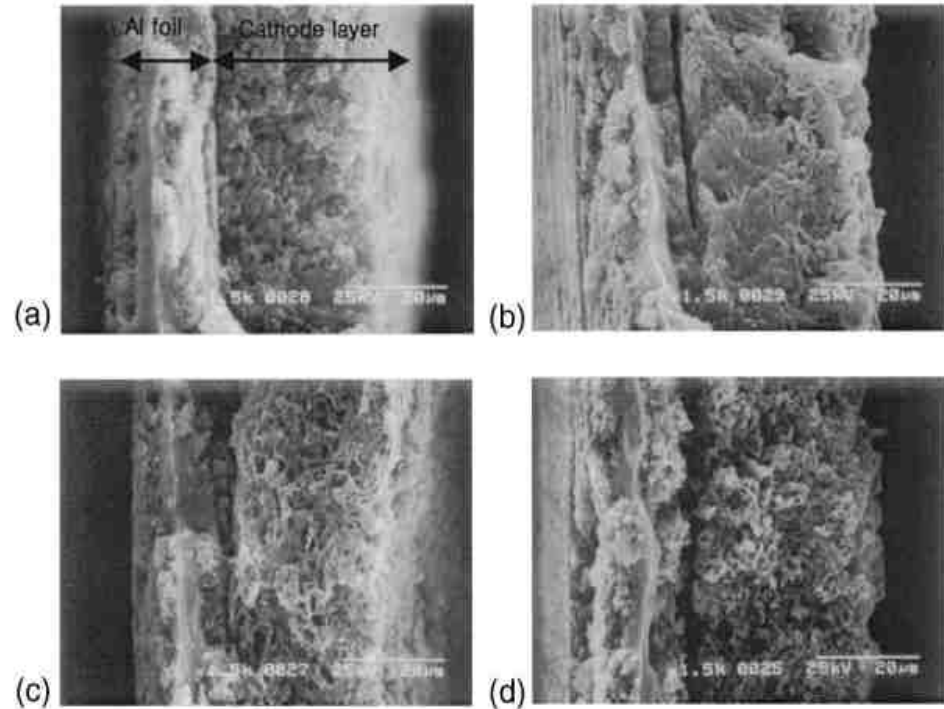
Still sulfur in separator at the end of discharge



# HETEROGENEITY OF REACTIONS ALONG THE CATHODE THICKNESS (2/2)

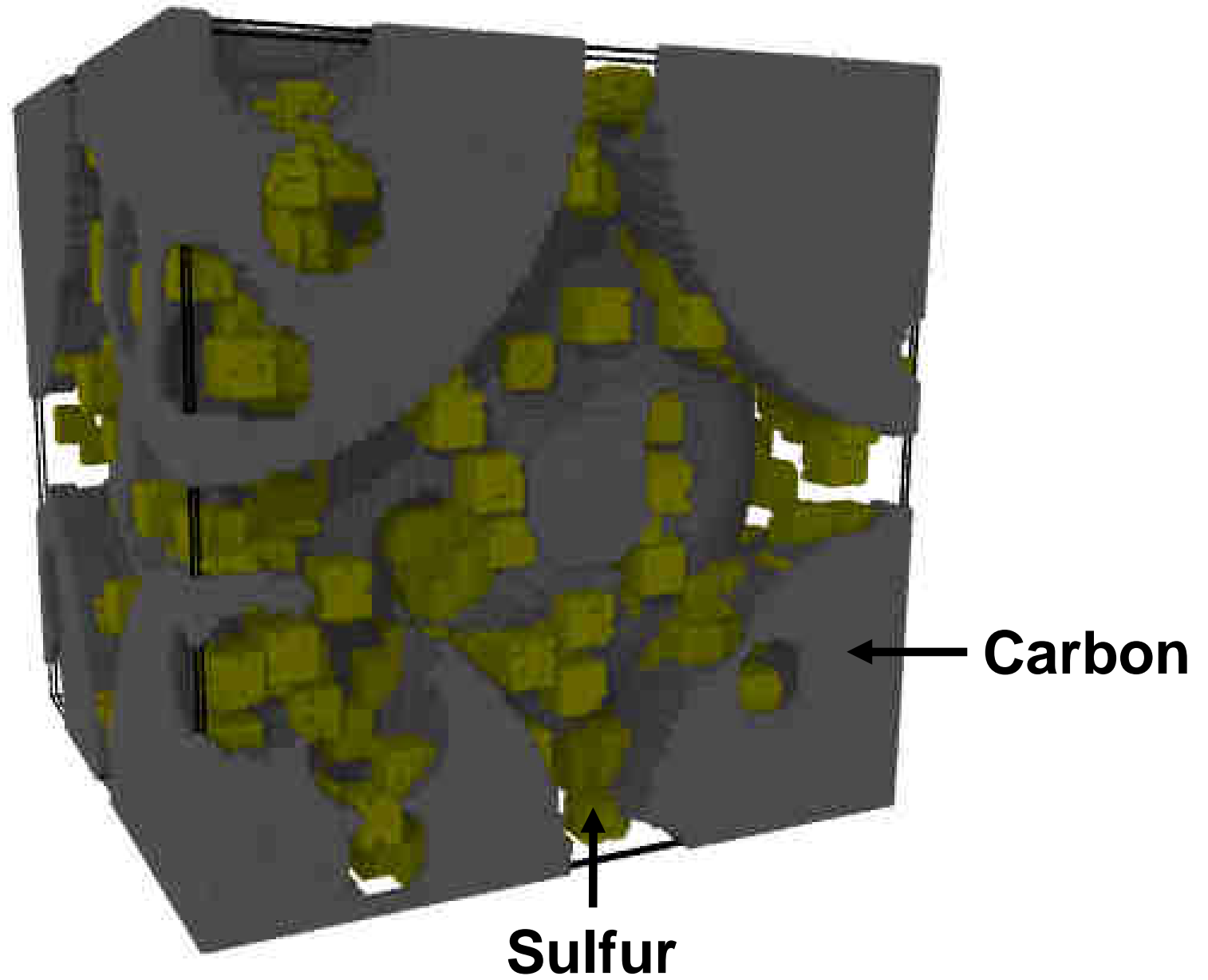


↳ Discharge stops due to clogging of the inter-particle pores.



**Figure 2.** SEM micrographs of the cross section of the sulfur cathodes (a) before discharge, (b) after discharge to 1.5 V at 0.26 mA/cm<sup>2</sup>, (c) after discharge to 1.5 V at 1.74 mA/cm<sup>2</sup>, and (d) after discharge to 1.5 V at 3.00 mA/cm<sup>2</sup>.





**PRISTINE Li-S CATHODE...**

# 3. REDOX FLOW BATTERIES



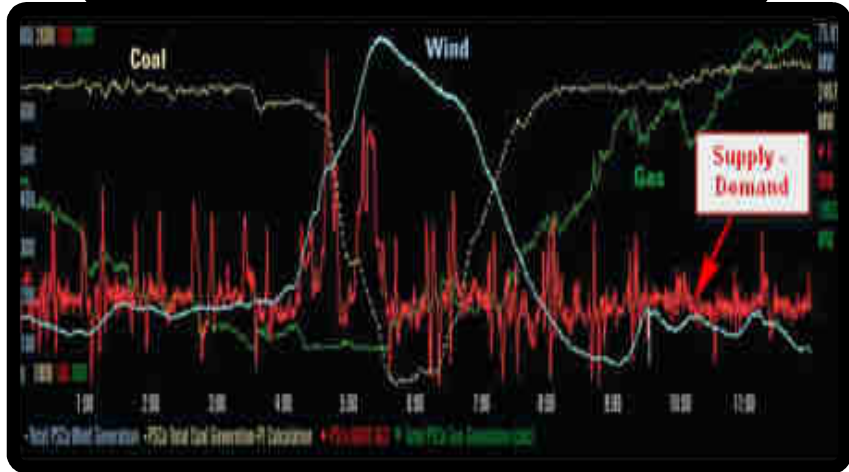


# STORING ENERGY FROM RENEWABLE SOURCES

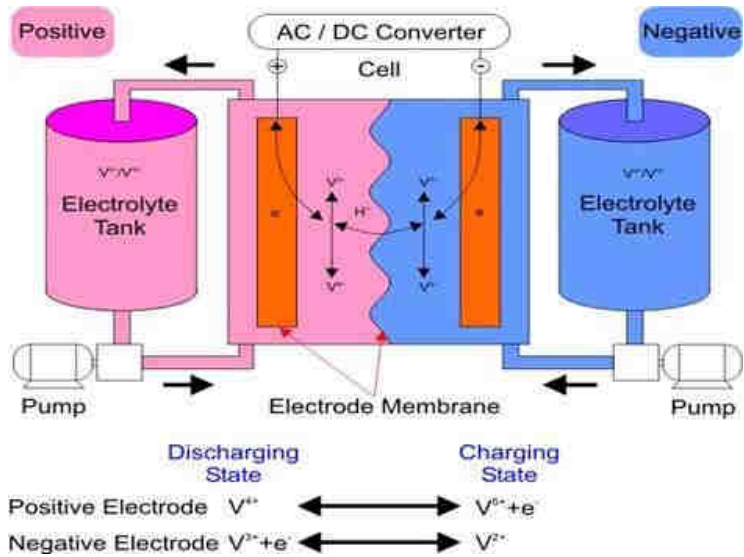
## Intermittent renewable energies



## Issues on grid management

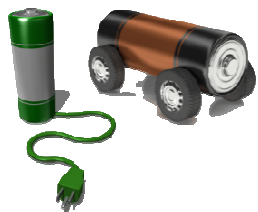


Public Service Co. of Colorado (PSCo) (July 2, 2008).



A. Z. Weber et al., Journal of Applied Electrochemistry **41** (10) (2011) 1137.

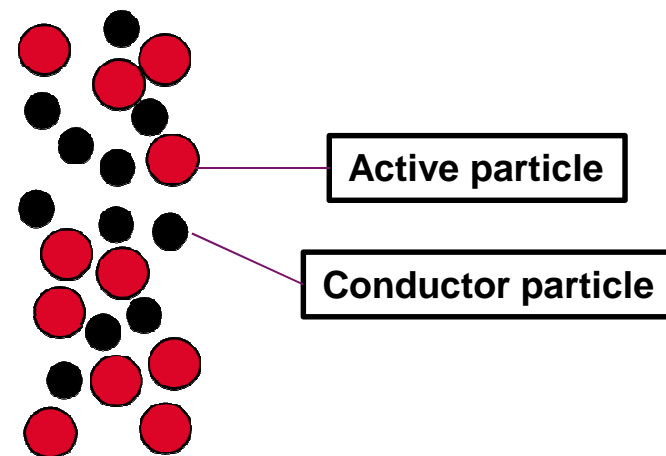
- ### Redox Flow Batteries
- ↳ High energy efficiency (85-90%)
  - ↳ Unlimited theoretical capacity
  - ↳ Long lifetime
  - ↳ Fast response time (millisecond)



# SLURRY-BASED REDOX FLOW BATTERIES (SRFB)

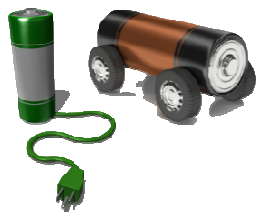
M. Duduta, B. Ho, V. C. Wood, P. Limthongkul, V. E. Brunini, W. C. Carter, Y.-M. Chiang, *Adv. Energy Mater.*, 1, 511 (2011).

Flow battery fueled by semi-solid suspensions of high-energy-density lithium storage compounds that are electrically “wired” by dilute percolating networks of nanoscale conductor particles.

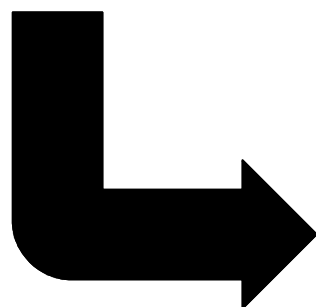
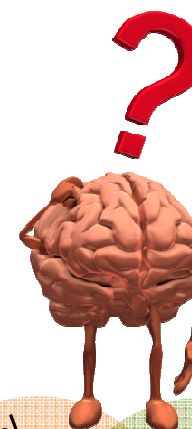
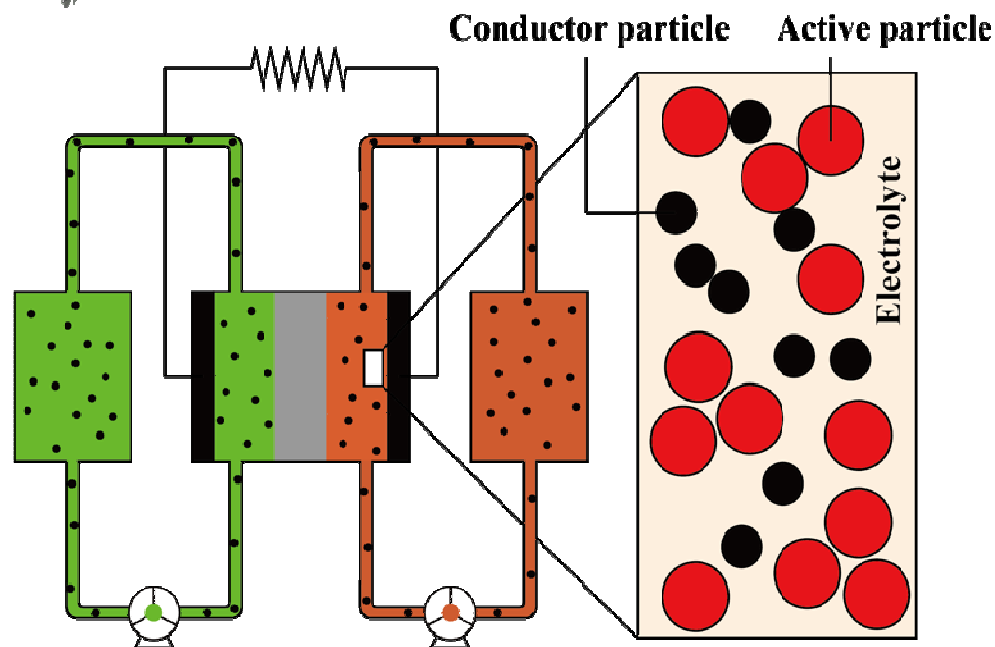


Prof. Alejandro A. Franco  
Mesostructure-performance relationships in batteries...  
*Pregl colloquium*  
NIC - Ljubljana, Slovenia  
December 14, 2016





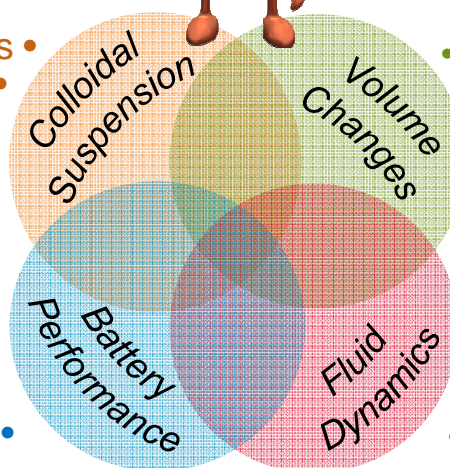
# SRFB: FUNDAMENTAL CHALLENGES (1/2)



## FUNDAMENTALS

- Interaction Energies
- Particle Wetting
- Stability
- Flocculation
- During Cycling

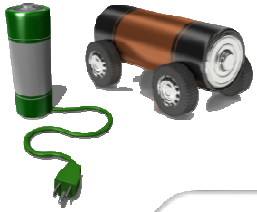
- Charge transfer
- Capacity
- Cyclability
- Degradation
- Side Reactions



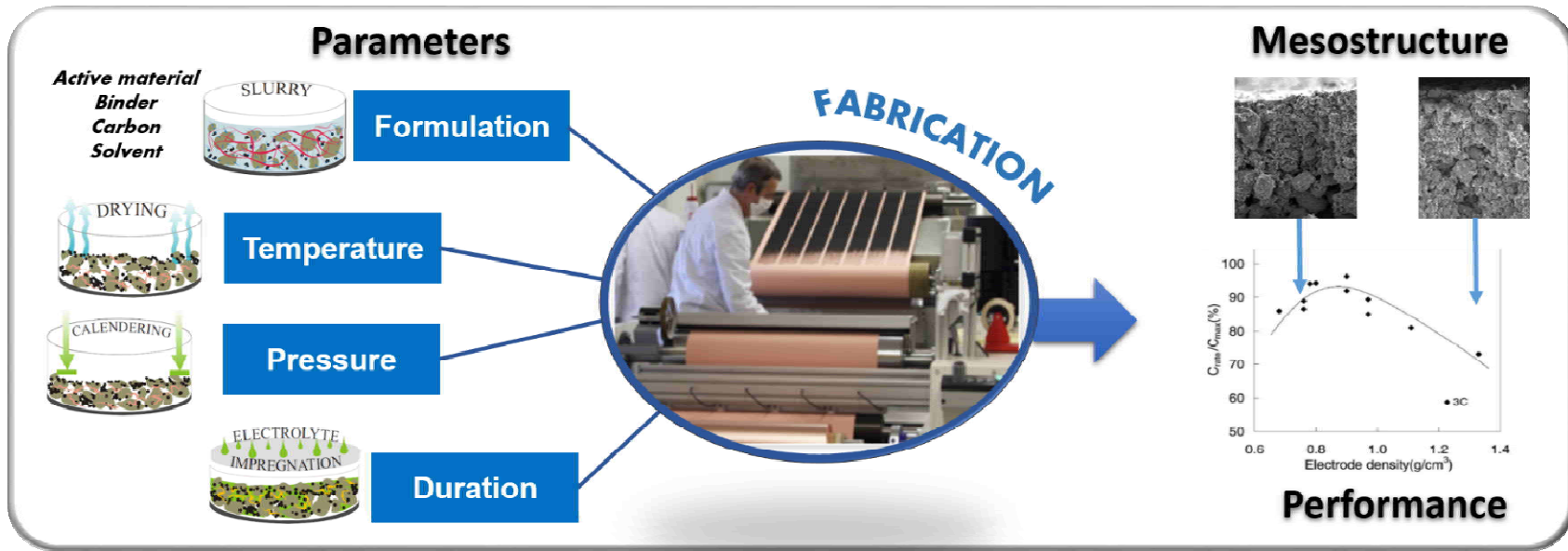
- Expansion Rate
- Disintegration
- Cracking
- SEI evolution
- Li conductivity

- Laminar Flow
- Energy Dissipation
- Density Variation
- Knudsen Number
- Networks Dynamics



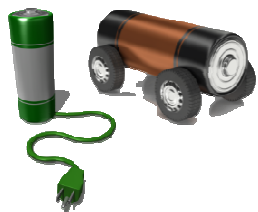


# MODELING OF BATTERIES FABRICATION



institut  
universitaire  
de France

Project started in  
October 2016

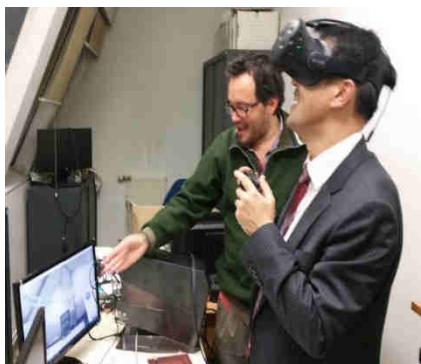
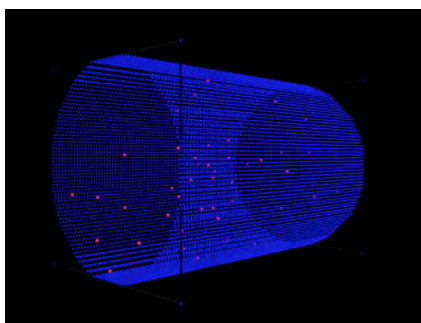


# TEACHING: USING IMMERSIVE VIRTUAL REALITY (VR)

Interactive Virtual Reality-based tool for energy storage teaching and immersive data analysis.

## Use in lectures within Master M.E.S.C.:

- ↳ Driving a Li-O<sub>2</sub>-powered Electric Car
- ↳ Tool informed by Kinetic Monte Carlo databases.



A.A. Franco, Y. Yin, R. Zhao, R. Lelong, I. Thouvenin, *J. Chem. Education*, in preparation (2016).





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- ❑ My students and postdocs



From left to right: R. Zhao, Dr. M. Quiroga, A. Torayev, G. Shukla, Y. Yin, A. Geng, Prof. A..A Franco, M. Maiza, V. Thangavel, R. Andersson, C. Gaya, A. Shodiyev.

Amiens cathedral by night



FUNDING



# THANK YOU

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